

A 3D simulation of an injection molding process. A white plastic mold is shown in a semi-transparent view, revealing a yellow molten plastic being injected into a cavity. The plastic is shown as a bright yellow stream entering from the right and filling the mold. The mold is set against a light gray background with a subtle grid pattern.

Autodesk Society of Rheology Meeting: May 2013

Challenges in the Simulation of Injection Molding

Dr. Franco Costa

Senior Research Leader – Autodesk Simulation (Moldflow)



Content

■ Autodesk Simulation Overview

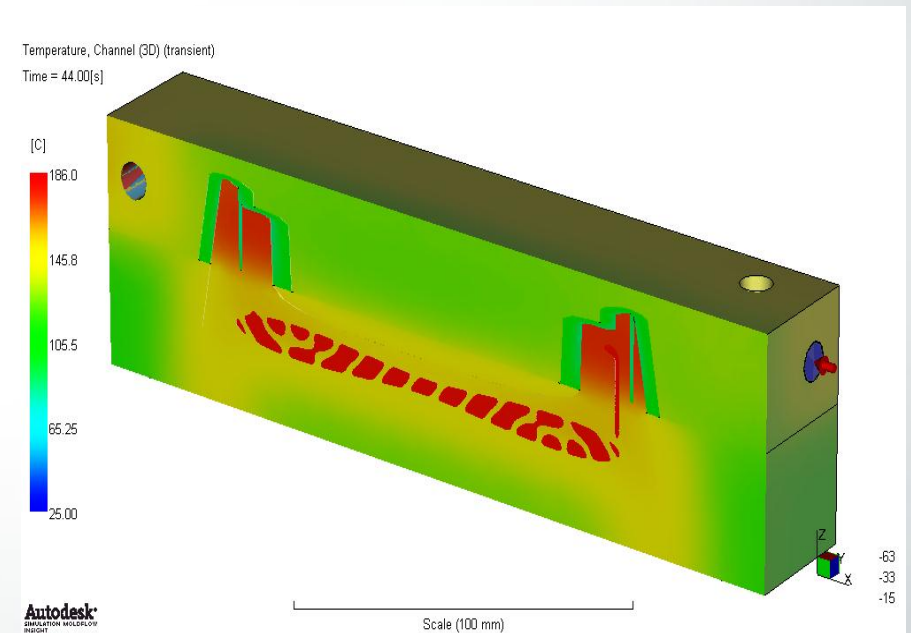
- Product Overview
- Material Characterization

■ Some Recent Advances

- Long Fiber Breakage
- Crystalline Morphology
- Stress Relaxation

■ Some Tough Problems

- Micromolding
- Flow imbalances + Ear-flow
- Jetting Flows
- Tiger Stripes



Autodesk Simulation Investments

\$500M+
Simulation
Investment

2005

SOLID
Dynamics

PLASSO

Robobat®

 **GREEN**
BUILDING STUDIO

 ECOTECK

Moldflow®

 **ALGOR®**

 Fatigue Wizard

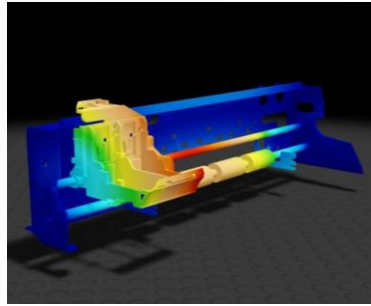
 **cfdesign®**
Upfront CFD

FIREHOLE
COMPOSITES

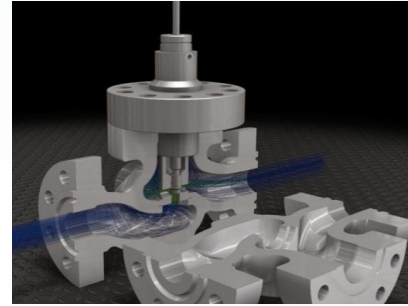
230+ Direct
Development
Staff

Today

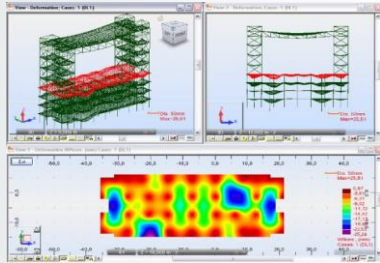
FEA



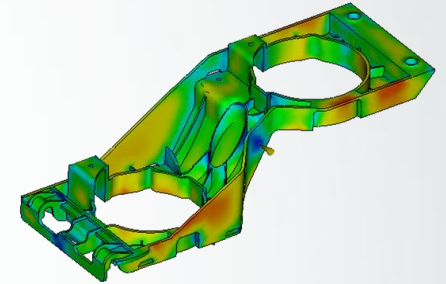
CFD



Structural /
Code Checking



Manufacturing



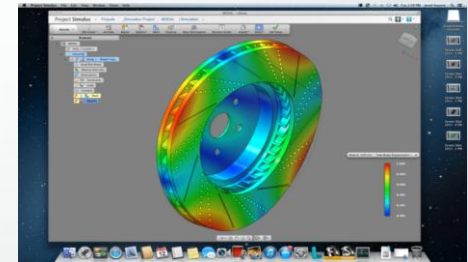
Test and Validation



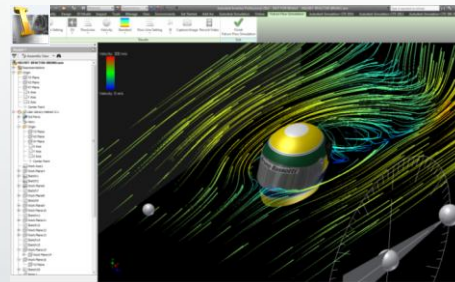
Mobile



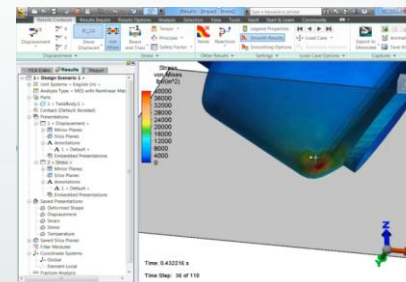
Cloud



Embedded

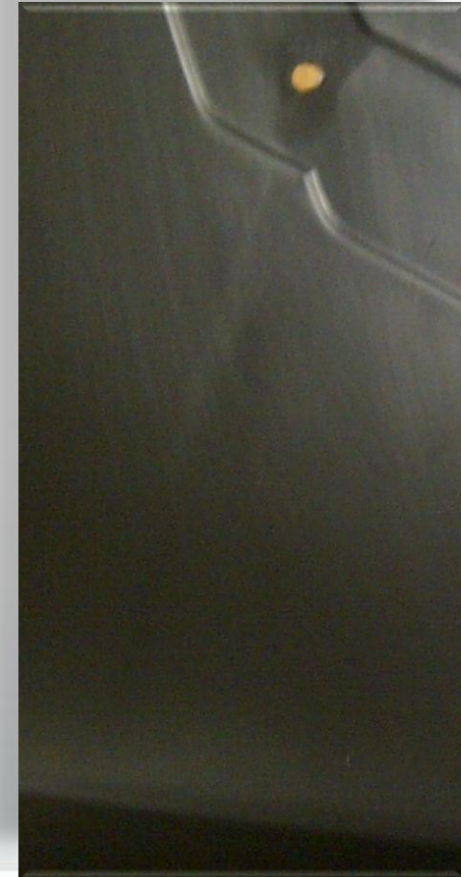


Desktop



Injection Molding

- Unlike other processes, may not be able to overcome problems with change of process conditions
- Simulation adds high value

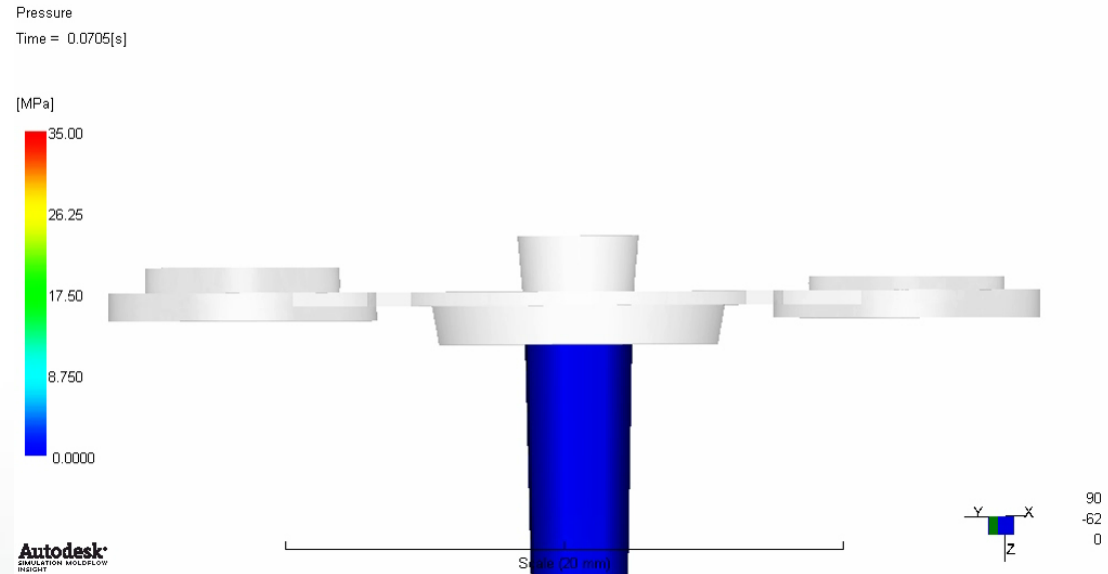


Plastic Flow Simulation

Simulate the flow of melted plastic to help optimize part and mold designs, reduce potential part defects, and improve the molding process

Features

- Filling and Packing Analysis
- Molding Window Analysis
- Design of Experiments
- Insert Overmolding
- Two-Shot Sequential Overmolding
- Compression and Injection-Compression Molding

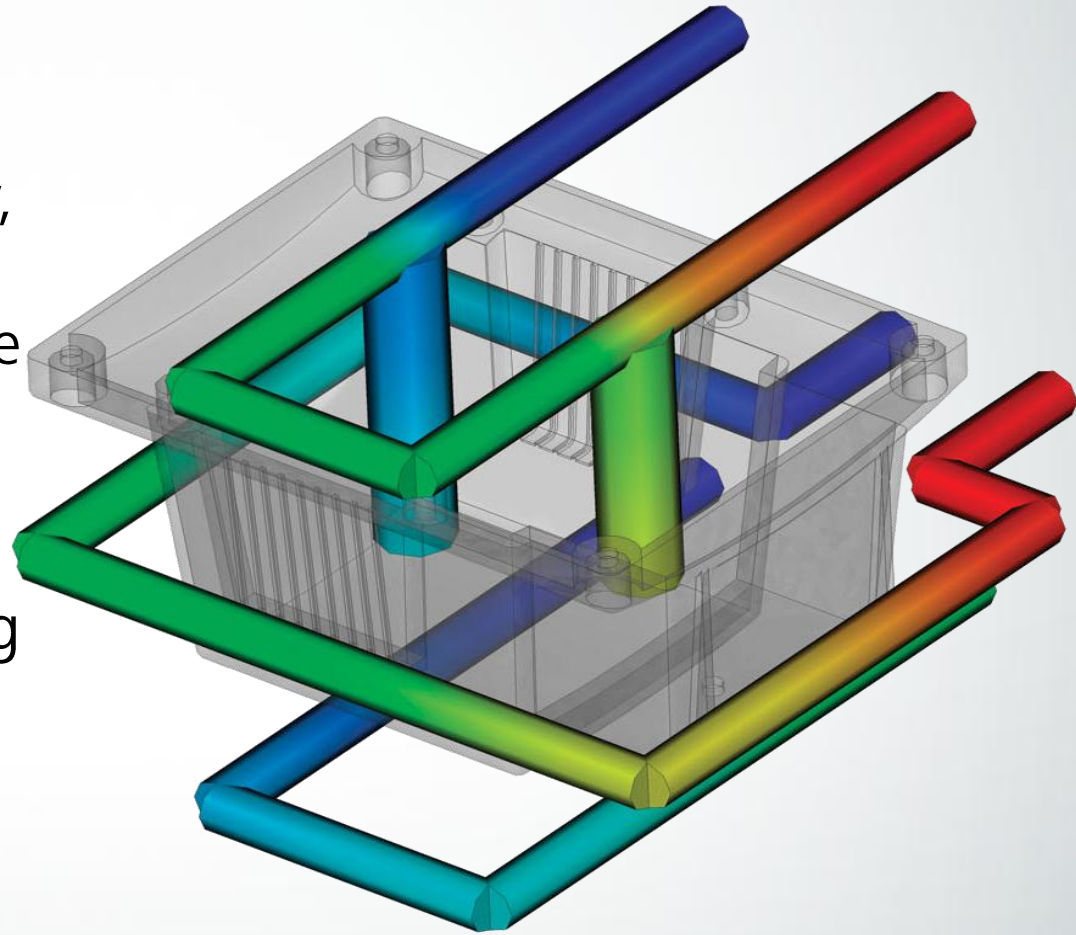


Mold Heating & Cooling Simulation

Improve cooling system efficiency, minimize part warpage, achieve smooth surfaces, and reduce cycle times

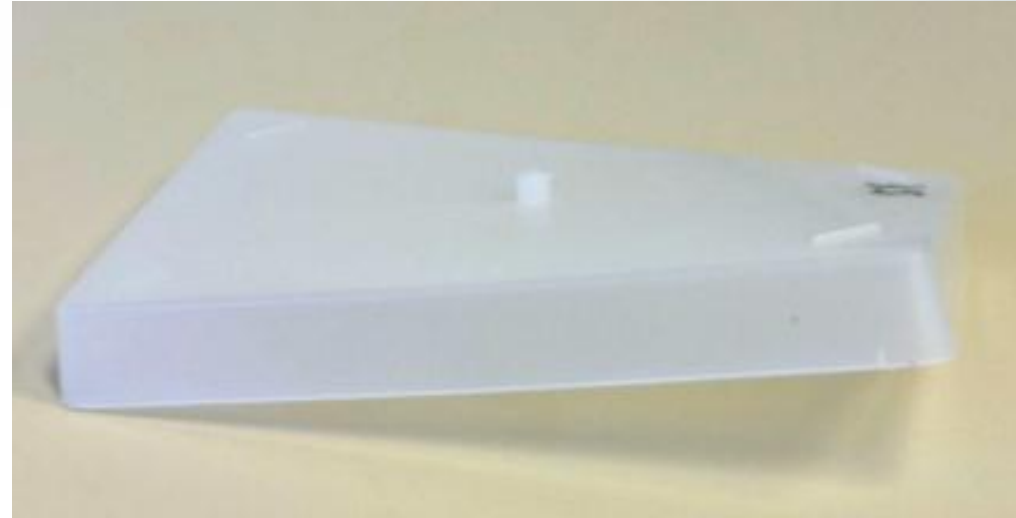
Features

- Cooling Component Modeling
- Cooling System Analysis
- Rapid Heat Cycle Molding



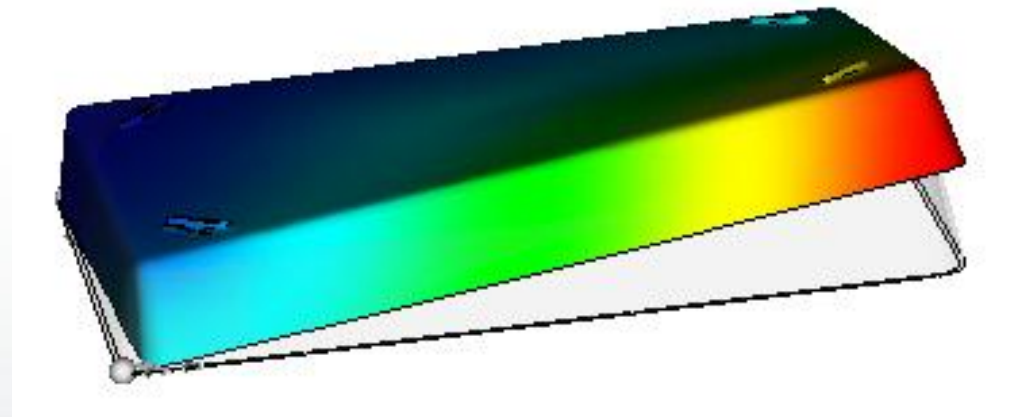
Shrinkage and Warpage Simulation

Predict and control post-molding shrinkage and warpage and evaluate the structural integrity of the molded part



Features

- Shrinkage Analysis
- Warpage Analysis
- Core Shift Control
- Fiber Orientation



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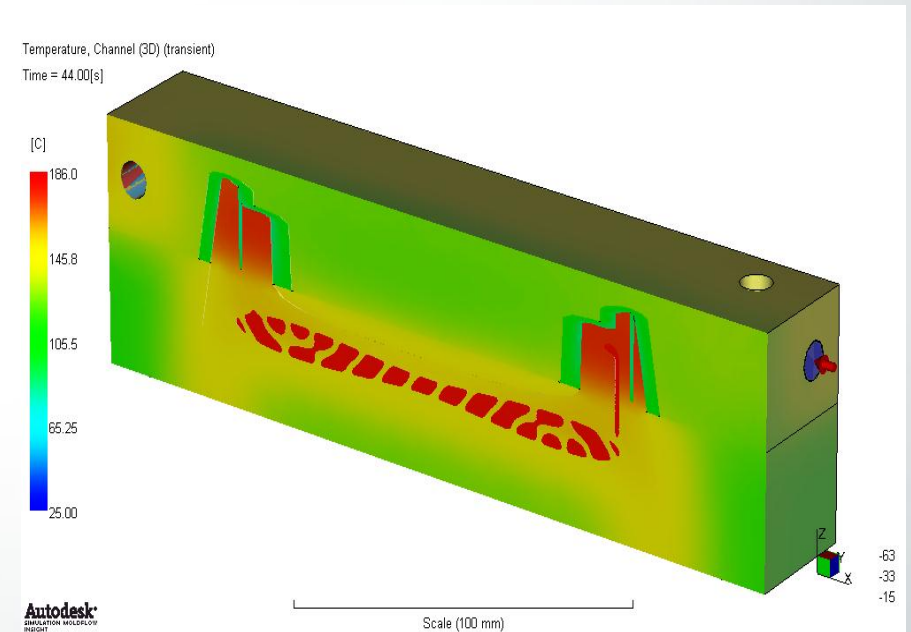
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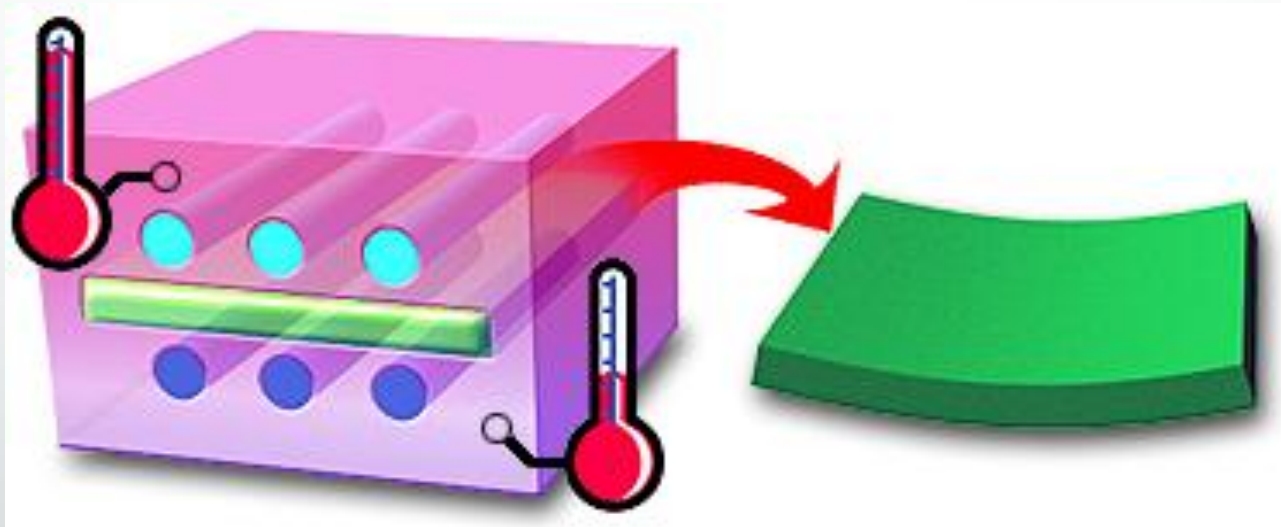
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Viscosity in Injection Molding

- Injection pressures range from 0-200MPa
- Shear rates range from 1-100,000/s
- Temperatures range from melt (300C) to mold (40C)
- The phase change from melt to solid must be identified for residual stress calculations



Rheological model - Modified Cross-WLF model

- Cross model captures the shear rate sensitivity of most material families
- WLF equation captures Arrhenius and hyperbolic temperature sensitivities depending on the magnitude of $T-T^*$

$$\eta = \frac{\eta_0}{1 + \left(\frac{\eta_0 \dot{\gamma}}{\text{Tau}^*} \right)^{(1-n)}}$$

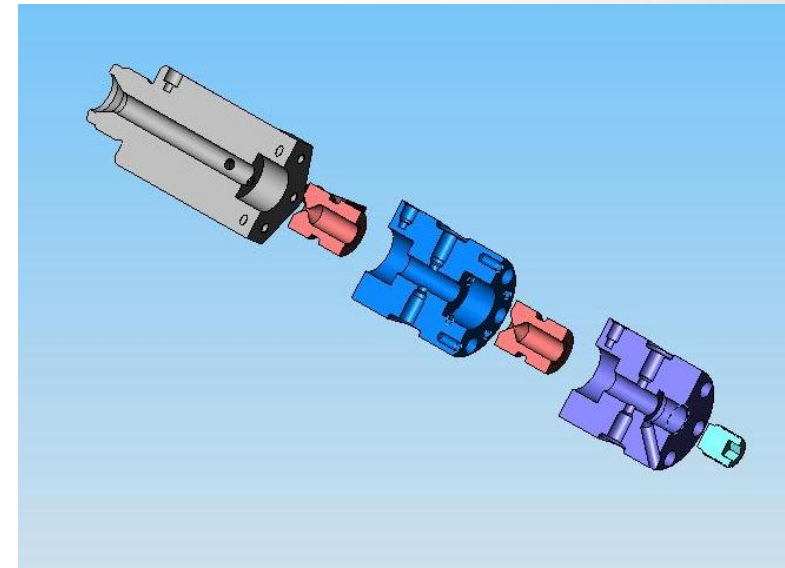
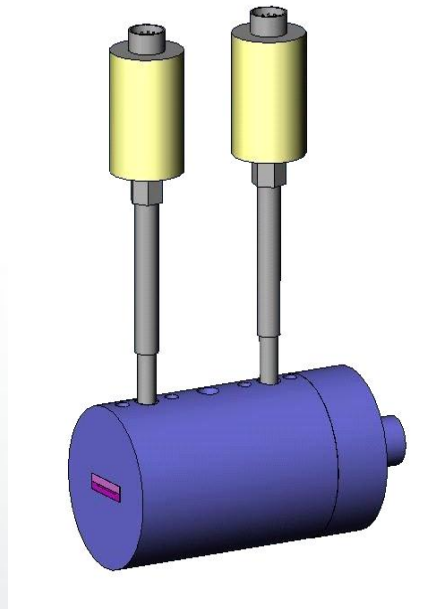
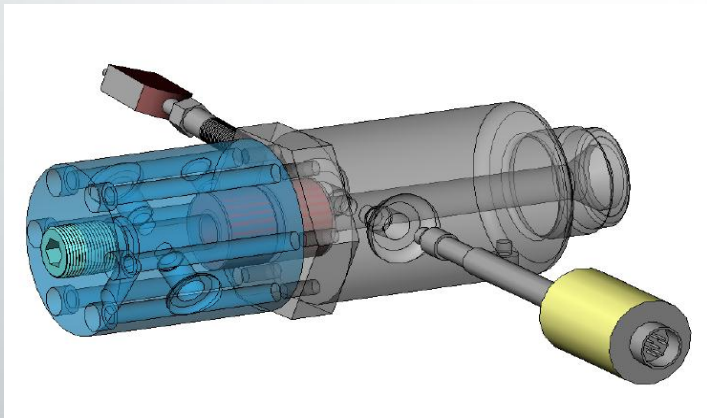
$$\eta_0 = D1 \exp \left[\frac{-A1 (T - T^*)}{A2 + (T - T^*)} \right]$$

where:

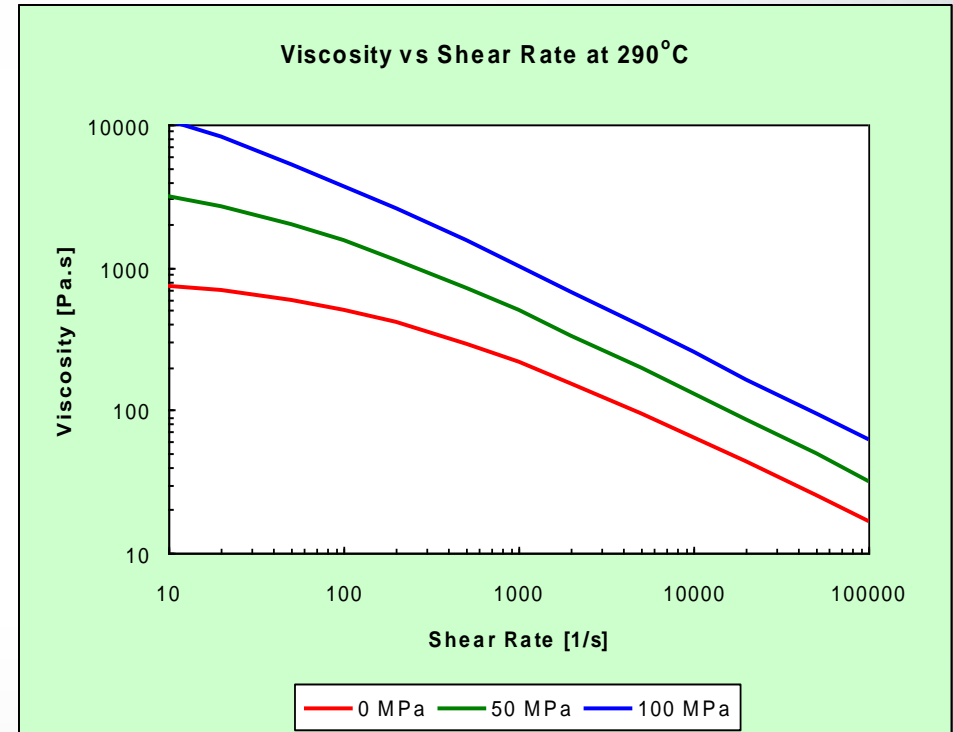
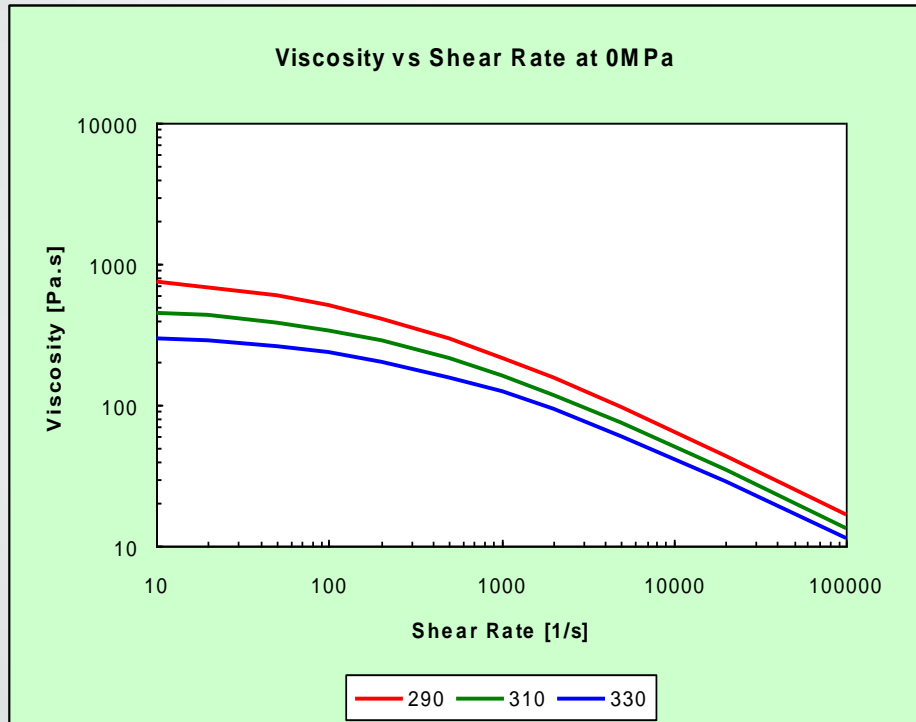
- $T^* = D2 + D3P$
- η is Viscosity (Pa. sec.)
- $\dot{\gamma}$ is Shear Rate (1/sec.)
- T is Temperature (deg.K)
- P is pressure (Pa)
- Unknowns: $D1, D2, D3, A1, A2, \text{Tau}^*, n$
- $A2 = A2^{\sim} + D3P$

Rheometer - Design

- Many materials are sensitive to the melt preparation conditions
- An inline rheometer prepares the melt under the same conditions used in injection molding (strong thermomechanical history, short residence time)

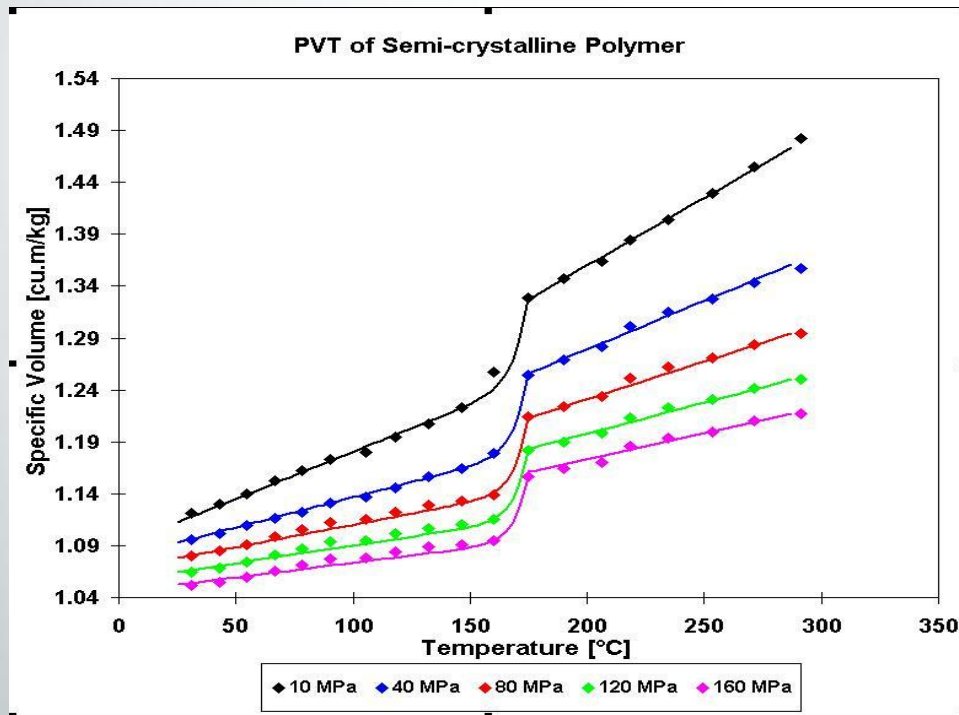


Rheometry – Pressure dependence



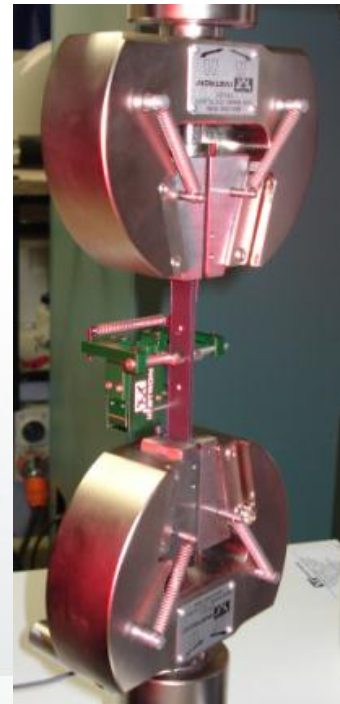
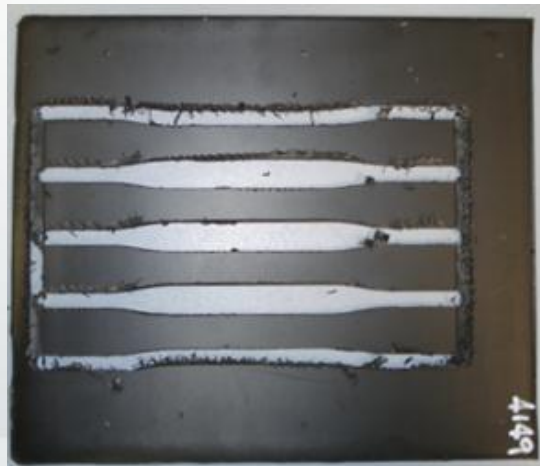
Compressibility - PVT

- Compressibility
 - High pressures involved
 - 0-200 MPa.
 - Materials are compressible



Testing Resources

- Injection Molding Machines
- Preparation
- Viscosity
- Thermal
- Pressure-Volume-Temperature
- Mechanical
- Shrinkage
- Viscoelasticity



Injection Molding Machines

Melbourne, Australia



Arburg 35 ton



Arburg 160 ton



Battenfeld 150 ton

Ithaca, NY, USA



Arburg 35 ton



2 * Krauss Maffei 160 ton

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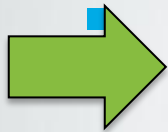
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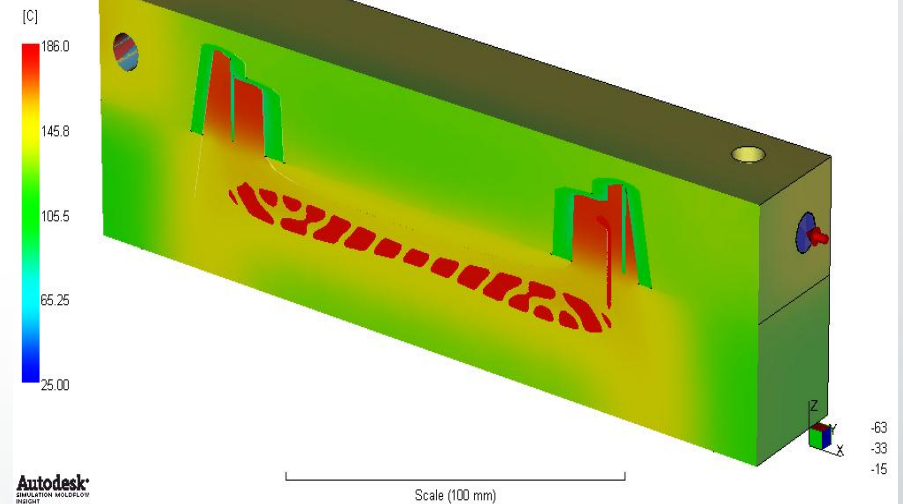
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Temperature, Channel (3D) (transient)
Time = 44.00[s]

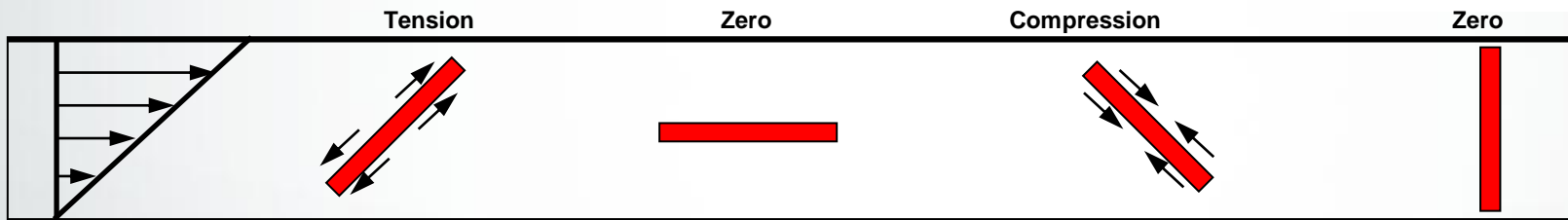


Fiber Breakage Model

- Phelps-Tucker Model
 - Probability of breakage of fibers length l_i

Dinh & Armstrong Model / Critical Buckling Force

$$F_i / F_{crit} = \frac{8\zeta\eta_m l_i^4}{\pi^3 E_f d_f^4} (D : A) > 1$$



$$\bar{P}_i = C_b \gamma \max\{0, [1 - \exp(1 - F_i / F_{crit})]\}$$

C_b : Strain Rate Coefficient Parameter

ζ : Dimensionless Drag Coefficient (Dg)

Fiber Breakage Model

- Probability of creating a fiber of length l_k from a fiber of length l_i

$$R_{ik} = G_{norm} \left(l_i, \frac{l_k}{2}, S l_k \right)$$

S: Distribution
Parameter

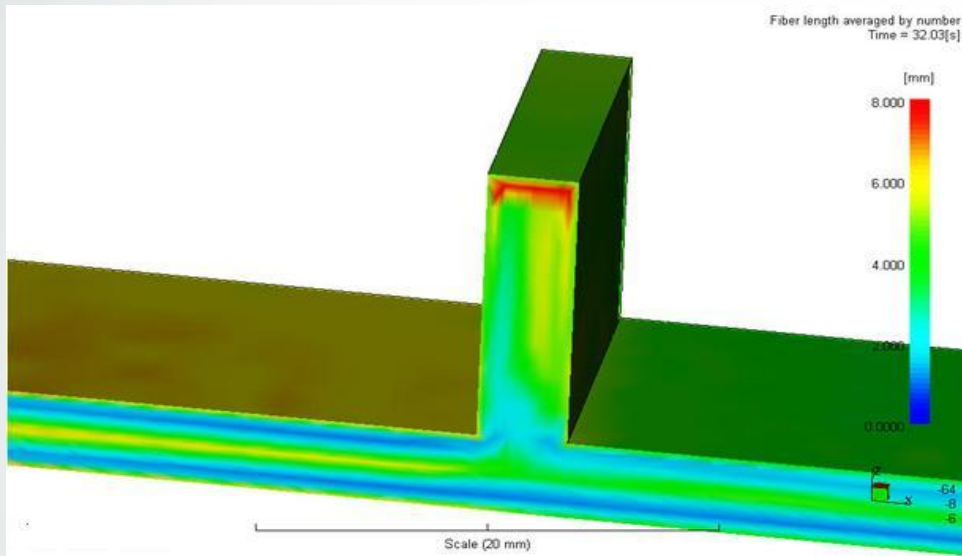
$\bar{N}_{i,t}$: Number of fibers of length l_i which exist at time t

$$\bar{N}_{i,t+\Delta t} = \bar{N}_{i,t} - \bar{P}_i \bar{N}_{i,t} \Delta t + \sum_{k|k \geq i}^M \bar{R}_{ik} \bar{N}_{k,t} \Delta t$$

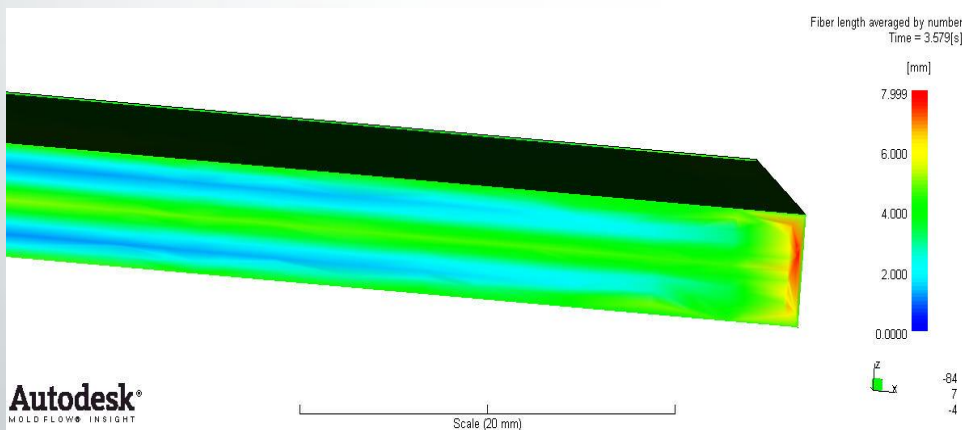
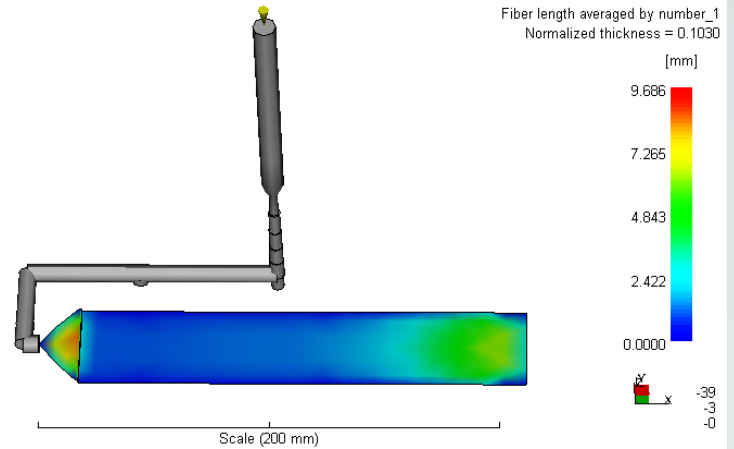
$i = 1, 2, \dots, M;$

Fiber Length Distribution in 3D

Some long fibers pushed to the end?

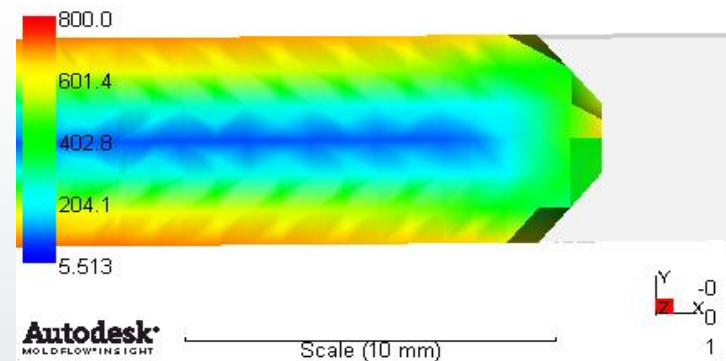


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MOLD FLOW INSIGHT



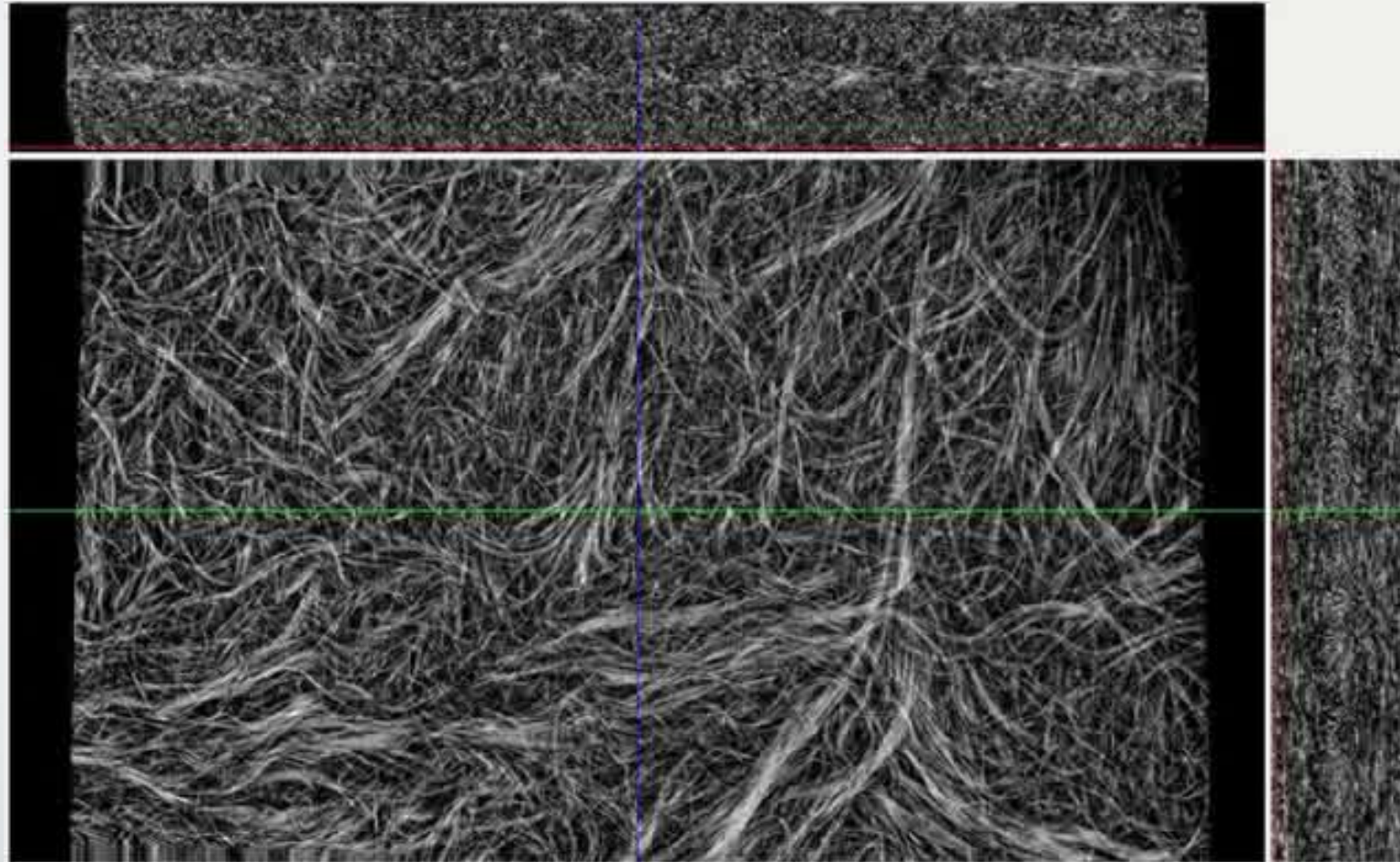
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MOLD FLOW INSIGHT

Shear rate
Time = 0.0871[s]
[1/s]



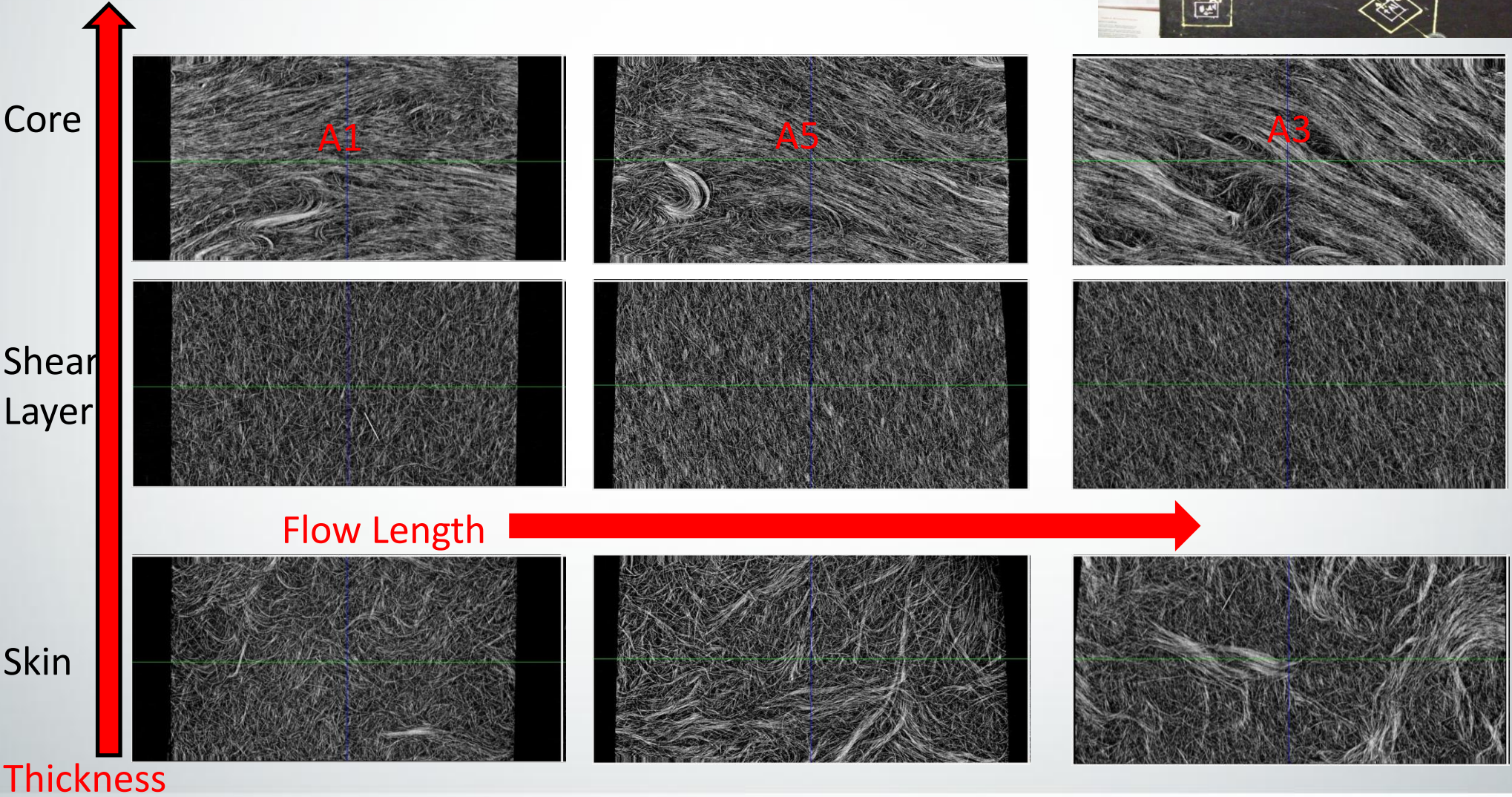
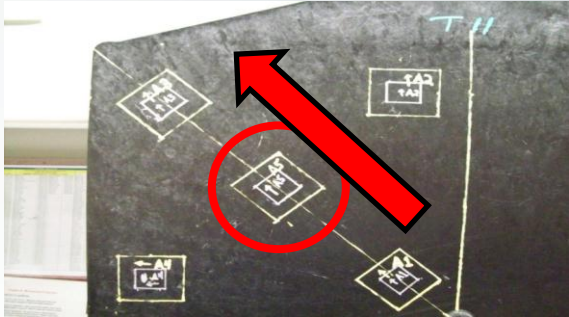
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MOLD FLOW INSIGHT

Fiber Length Distribution Measurement & Calculation – Ticona Moldings



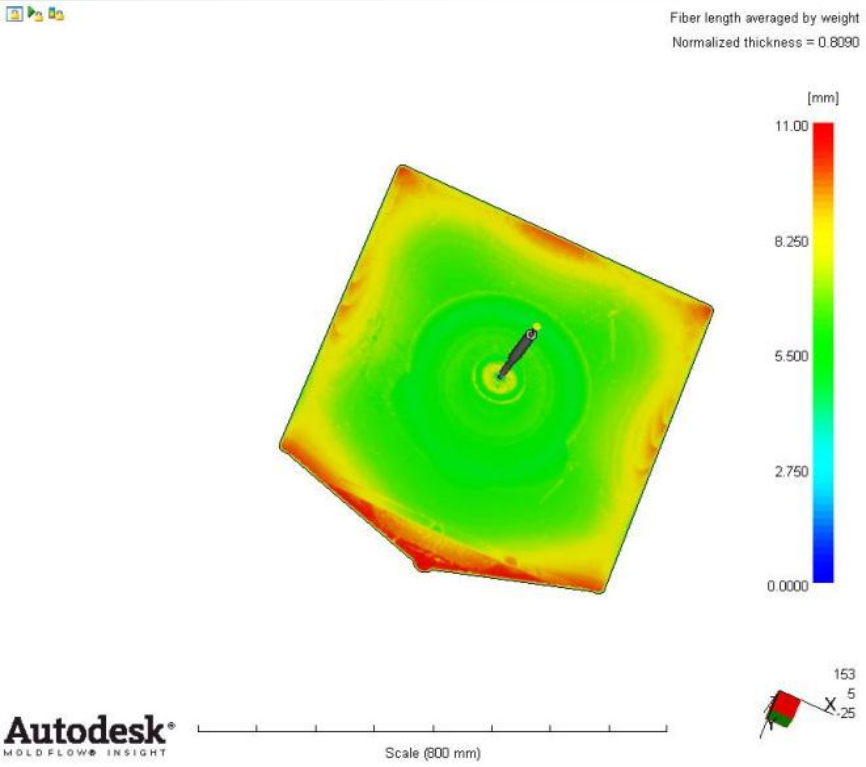
Skin

Long Fiber Breakage Model Fiber Length Evolution

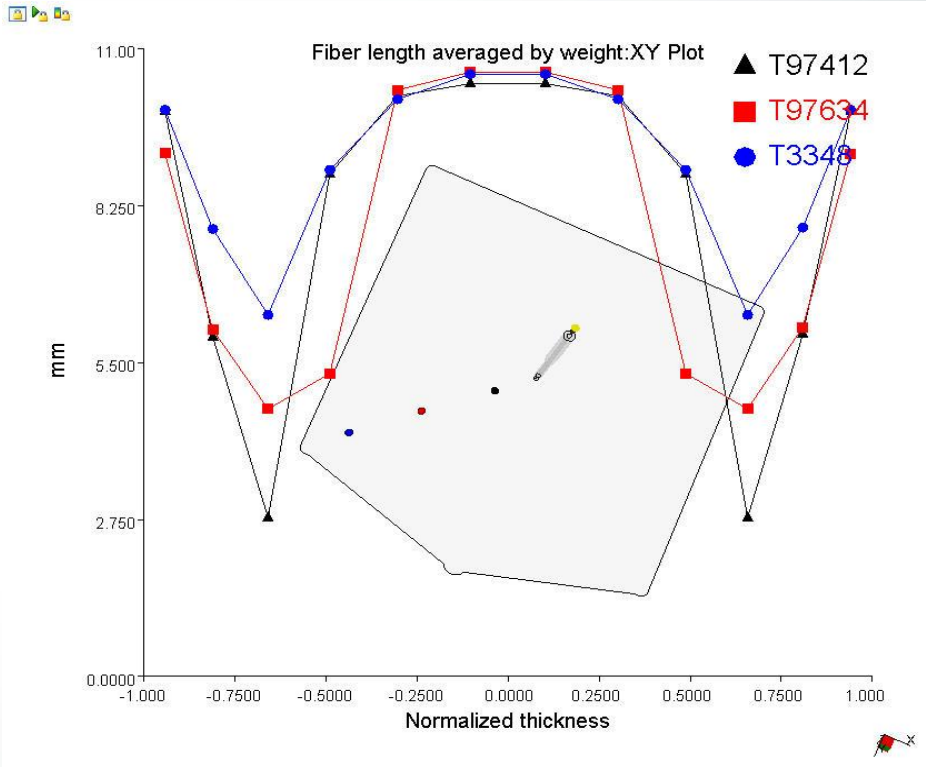


Courtesy: Ticona

Predicted Fiber Length Distributions



Midplane



3D

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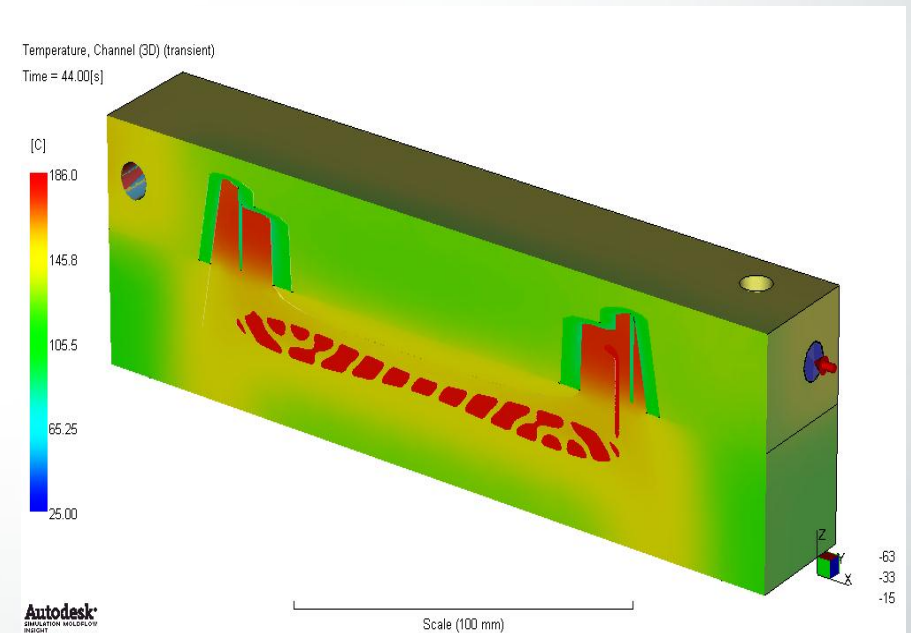
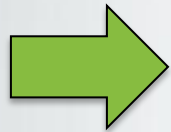
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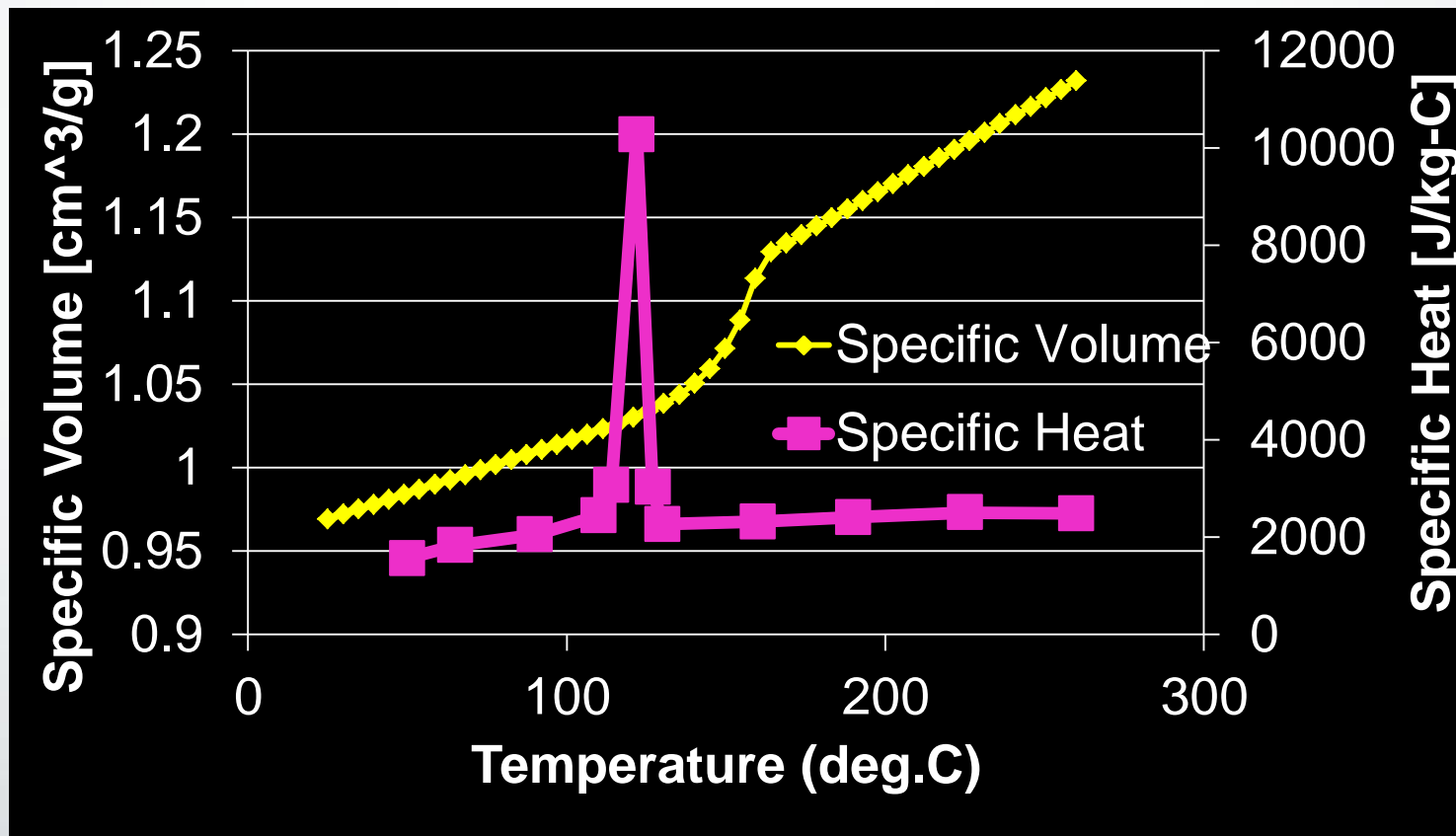
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Why Crystallization?

- Solidification
 - Single transition temperature?



Cooling Rate Effect on Solidification

Measured Specific Volume during cooling

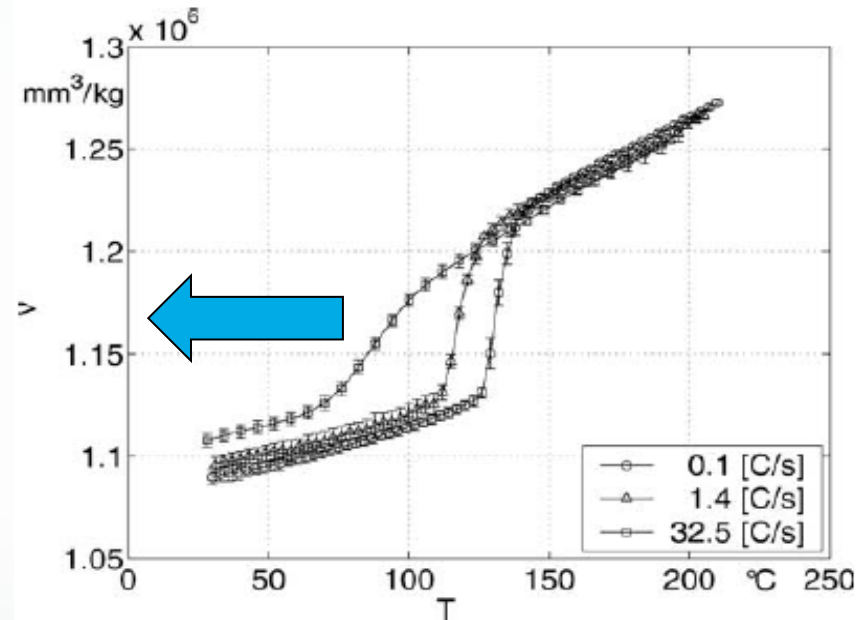


Fig. 9. Influence of cooling rate on the specific volume of i-PP at a pressure of 40 MPa. Average cooling rates during crystallization are given in the figure

van der Beek et. al. Inter. Polymer Processing, 20, 111-120, (2005).

Shear Rate Effect on Solidification

Measured Specific Volume during cooling after shearing

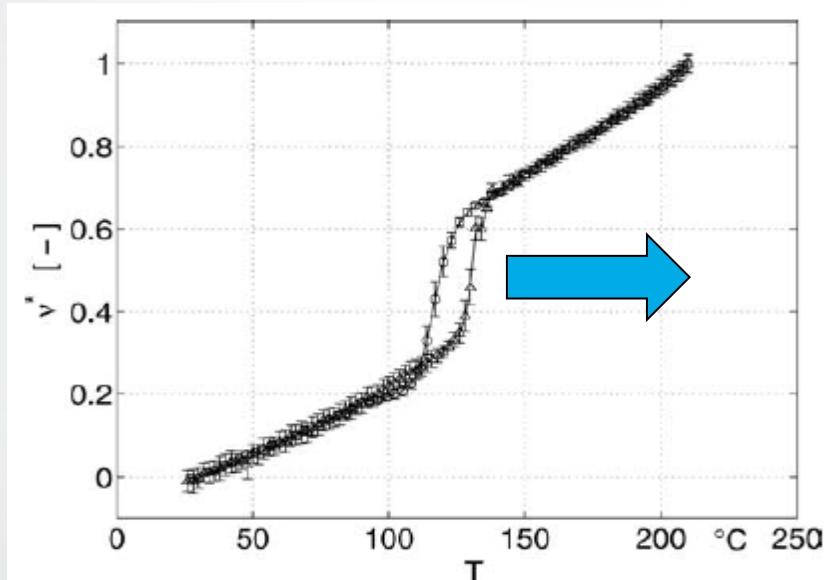


Fig. 10. Influence of shear flow on the normalized specific volume of i-PP. Shear is applied as a step function at 139°C, with a shear rate of 38.5 l/s to a total shear of 117. Specific volume with (\triangle) and without shear flow (\circ) is obtained at an average cooling rate during crystallization of 1.4°C/s and a pressure of 40 MPa



Image: IME Technologies

van der Beek et. al. Inter. Polymer Processing, 20, 111-120, (2005).

Model of crystallization kinetics

$$G(T) = G_0 \exp \left[-\frac{U^*}{R(T - T_\infty)} \right] \exp \left[-\frac{f \cdot K_g}{T(T_m^0 - T)} \right],$$

$$T_\infty = T_g - 30, \quad f = \frac{(T + T_m^0)}{2T}$$



G(T)

(Growth Rate)

$$N = N_0 + N_f$$

$$\ln N_0 = a_N (T_m^0 - T) + b_N$$

$$\dot{N}_f + \frac{1}{\lambda_N} N_f = f (\Delta F_f) T$$



N(T, ΔF_f)

(Nuclei number density)

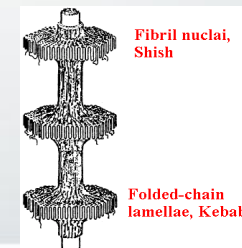
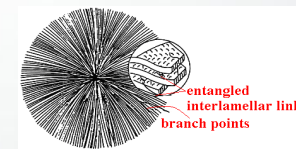
a_N, b_N, T_m^0, G_0 & K_g
Are determined from
DSC Experiments for
each material grade

Hadinata et al.
PPS 23

$$\phi = \frac{4\pi}{3} \int_0^t \dot{N}_0(s) \left[\int_s^t G(u) du \right]^3 ds$$

$$\psi = \pi \int_0^t \dot{L}_{total}(s) \left[\int_s^t G(u) du \right]^2 ds$$

$$\alpha = 1 - \exp [-(\phi + \psi)]$$



Crystallization Effect on Flow

- Calculate relative crystallinity (α) due to flow induced nucleation and temperature:

Viscosity

$$\eta(\dot{\gamma}, \alpha) = \eta_a \left(1 + \frac{(\alpha/A)^{\beta_1}}{(1-\alpha/A)^\beta} \right), \alpha < A$$

Specific Heat

$$c_p(\alpha, T) = \alpha c_{p_s}(T) + (1-\alpha) c_{p_a}(T)$$

Thermal Conductivity

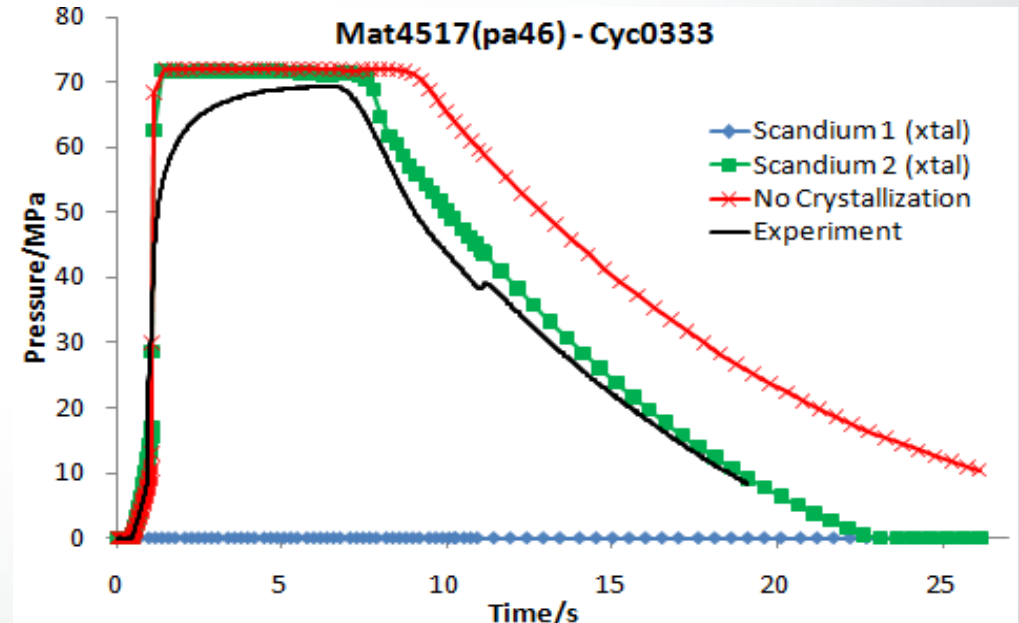
$$k(T) = \alpha k_s(T) + (1-\alpha) k_a(T)$$

Density

$$\nu = \alpha \nu_s(p, T) + (1-\alpha) \nu_a(p, T)$$

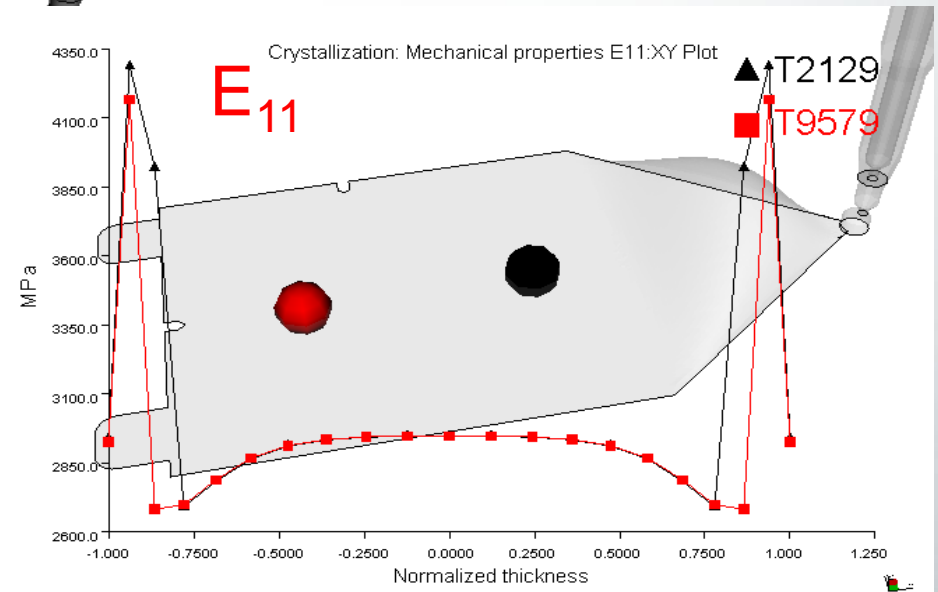
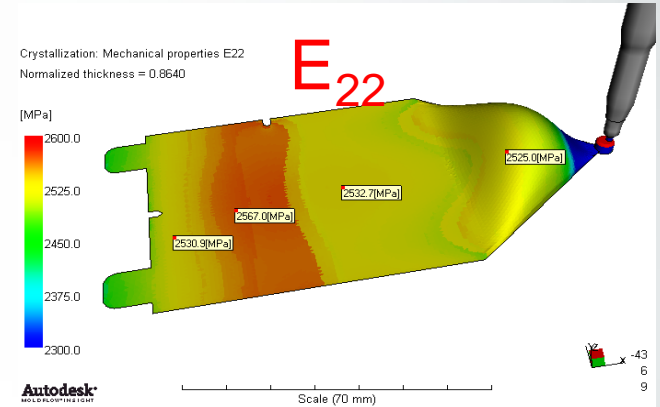
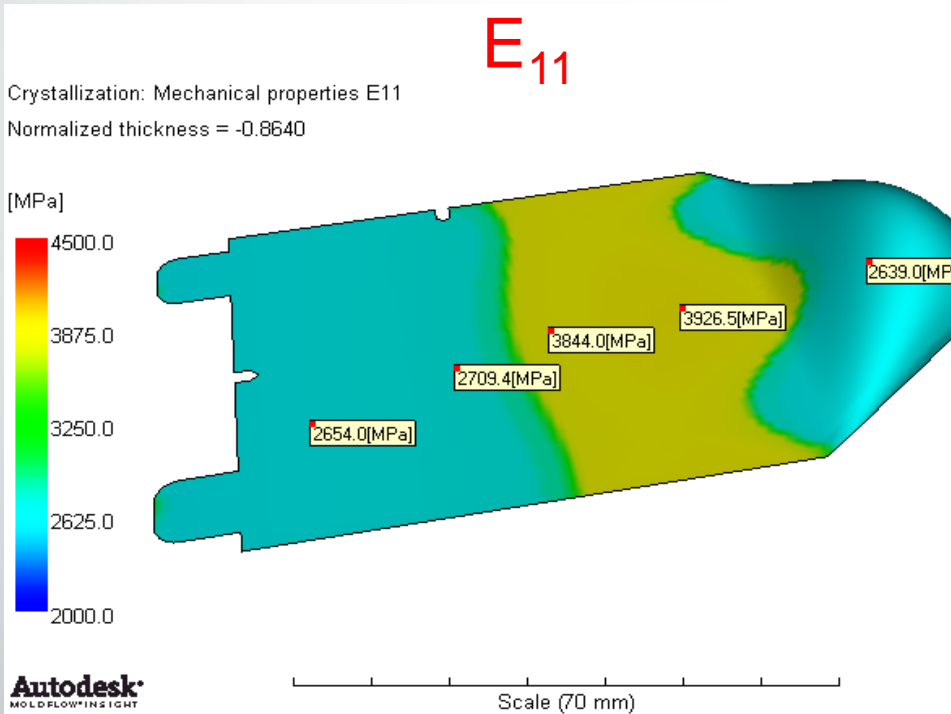
Temperature

$$\rho(\alpha) c_p(\alpha) \frac{DT}{Dt} = k(\alpha) \nabla^2 T + \boldsymbol{\sigma} : \mathbf{D} + \rho_c H_c \chi_\infty \frac{\partial \alpha}{\partial t} - \frac{T}{\rho(\alpha)} \frac{\partial \rho(\alpha)}{\partial T} \frac{Dp}{Dt}$$



Predicted Modulus, E_{11} & E_{22}

- Varies through thickness
- Resolved in flow direction



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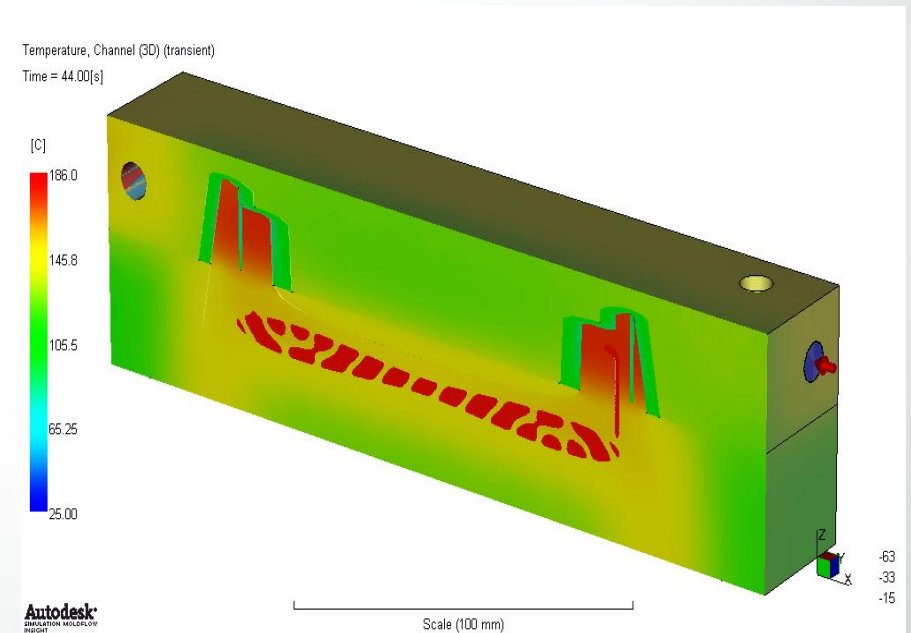
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Viscoelastic Warpage

Stresses arise from mechanical and thermal strains according to the a viscoelastic stiffness tensor

$$\sigma_{ij} = \int_0^t c_{ijkl} (\xi(t) - \xi(t')) \left(\frac{\partial \epsilon_{kl}}{\partial t'} - \alpha_{kl} \frac{\partial T}{\partial t'} \right) dt'$$

↑ ↑ ↑ ↑

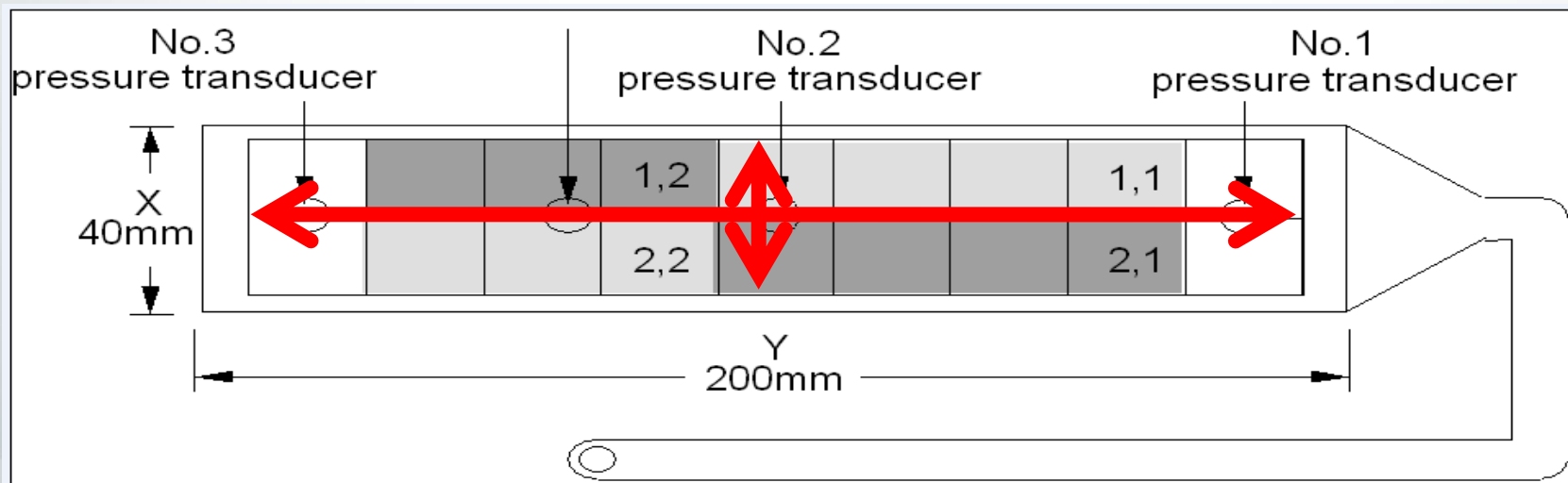
Residual Stiffness Mechanical Thermal
Stress tensor Strains Strains

The stiffness tensor changes according to time and temperature

$$F(t) = \sum_{k=1}^N g_k \exp\left(-\frac{t}{\lambda_k}\right)$$

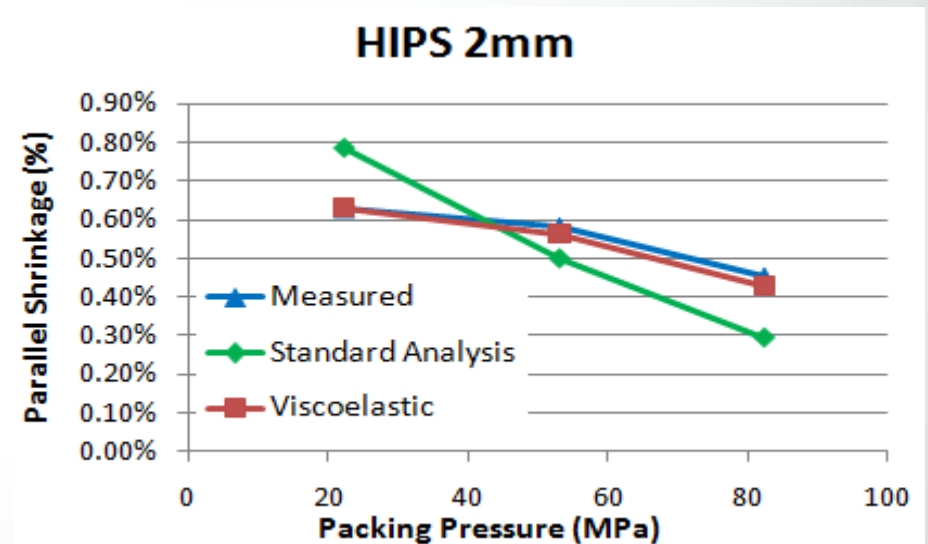
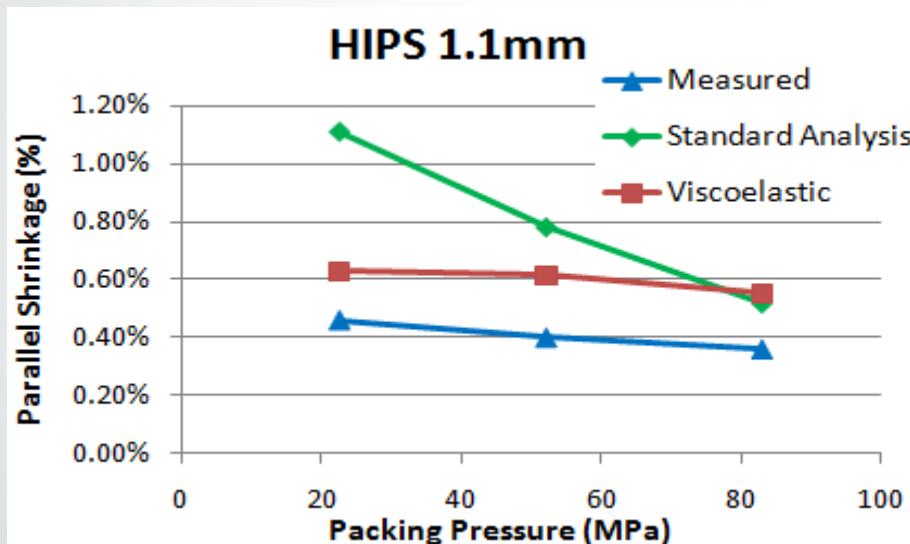
Viscoelastic Warpage for MP and DD

- Implemented in Midplane and Dual-Domain in Scandium Technology Preview
- Requires viscoelastic material data to be measured
- Viscoelastic simulation gives more realistic process sensitivity to packing pressure and packing/cooling time variation
- Validate using Shrinkage molding data



Viscoelastic Warpage on Tagdie Moldings

Examine trend with respect to Packing Pressure variation



Uncorrected (no CRIMS) shrinkage in the flow direction for an Amorphous non-fiber material. (HIPS)
Perpendicular Shrinkage shows a similar trend.

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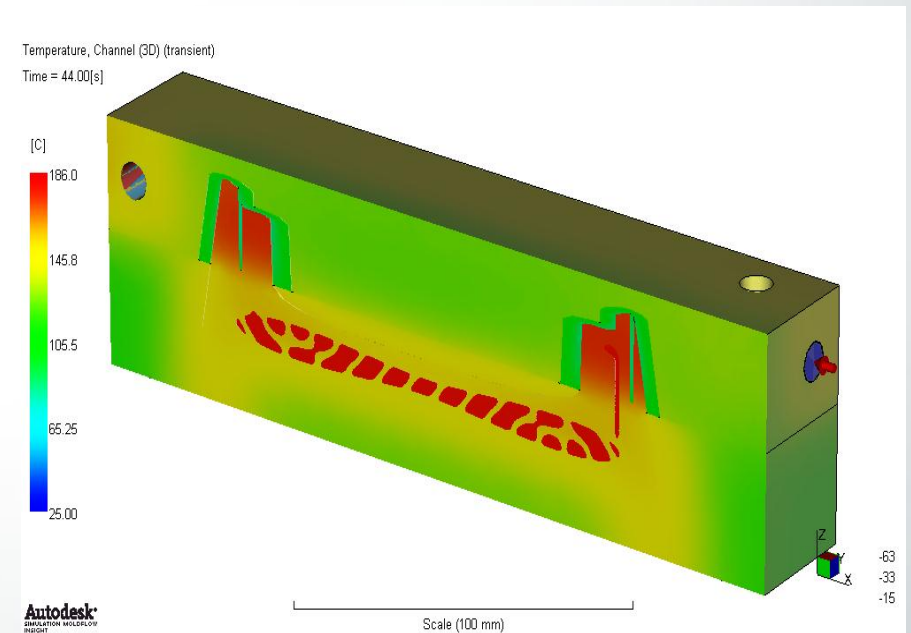
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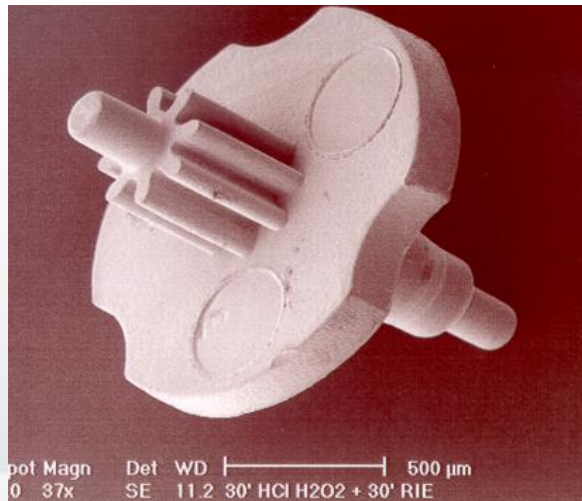
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Micro Moulding Validation Challenges

- Conventional sensors are large in comparison to the part
- High speed of the moulding process
- Non-conventional injection moulding machines & mechanisms
- Emergence of additional physical phenomena
 - ⇒ Scale effects emerging at micro scale
 - Wall-slip ?
 - Changed heat transfer coefficient between polymer and mould
 - Surface tension ?



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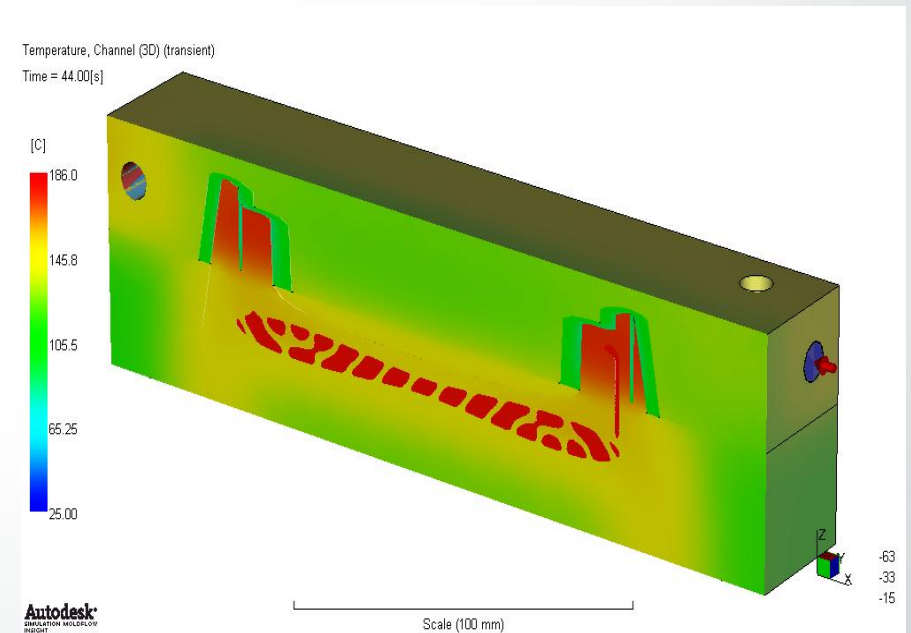
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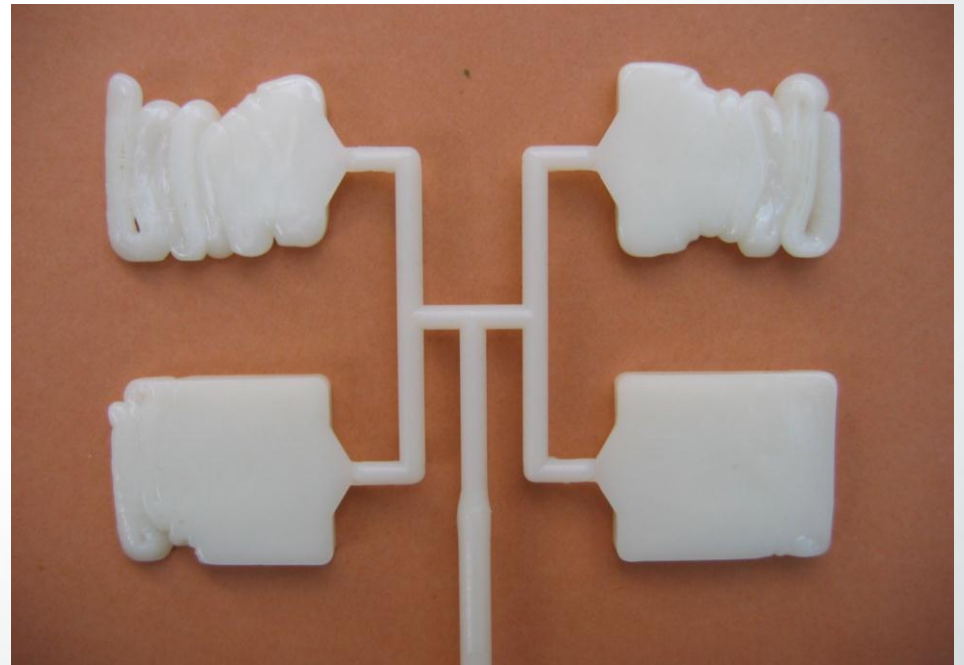
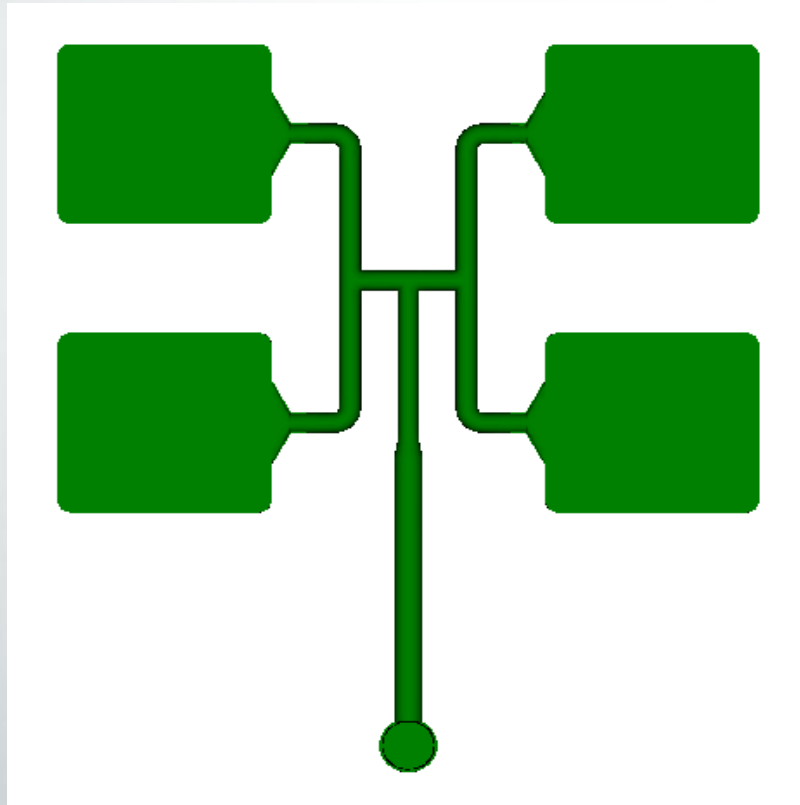
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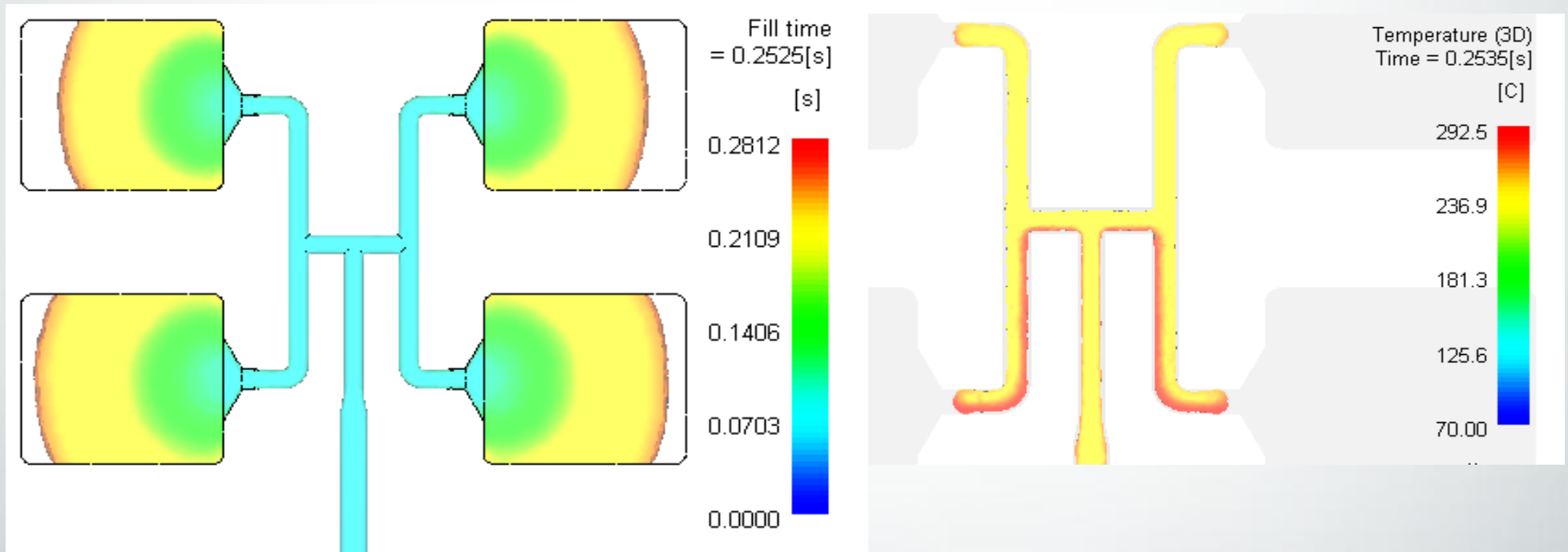
Runner imbalance: Test mold

- Often observe imbalance in symmetric part
- Due to shear heating - convection pattern



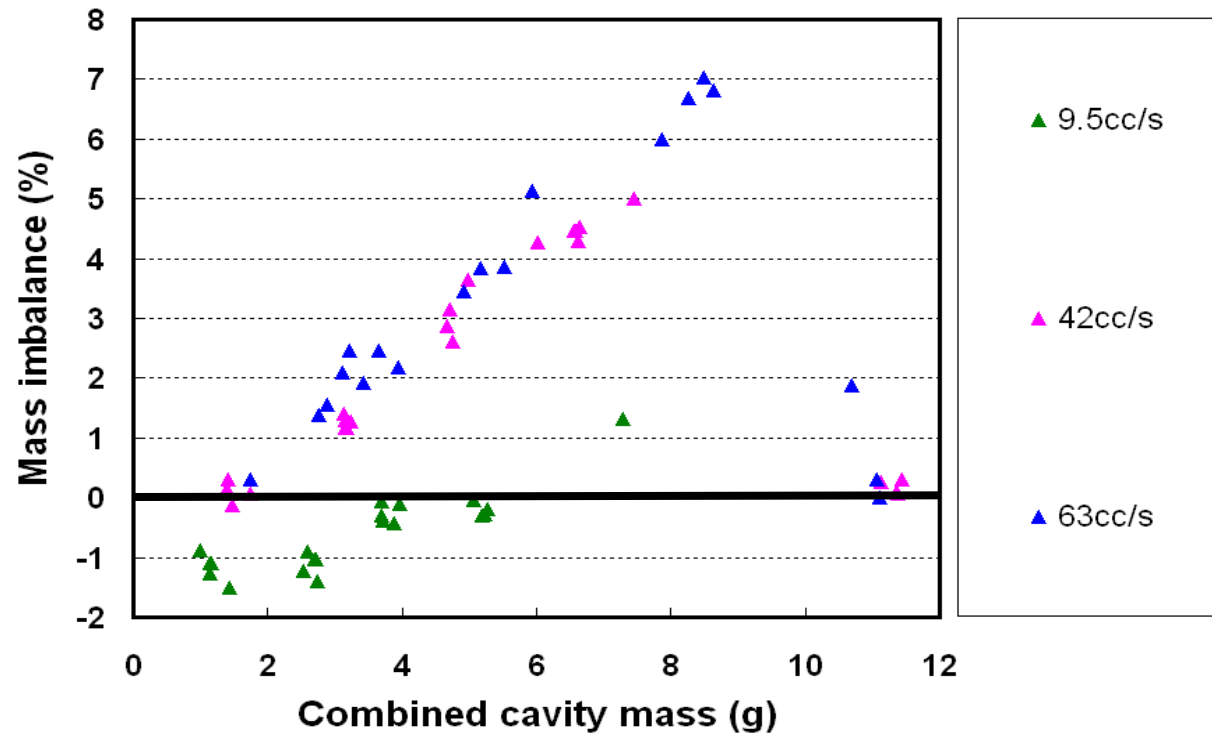
Runner imbalance: Fast injection

- Often observe imbalance in symmetric part
- Due to shear heating - convection pattern



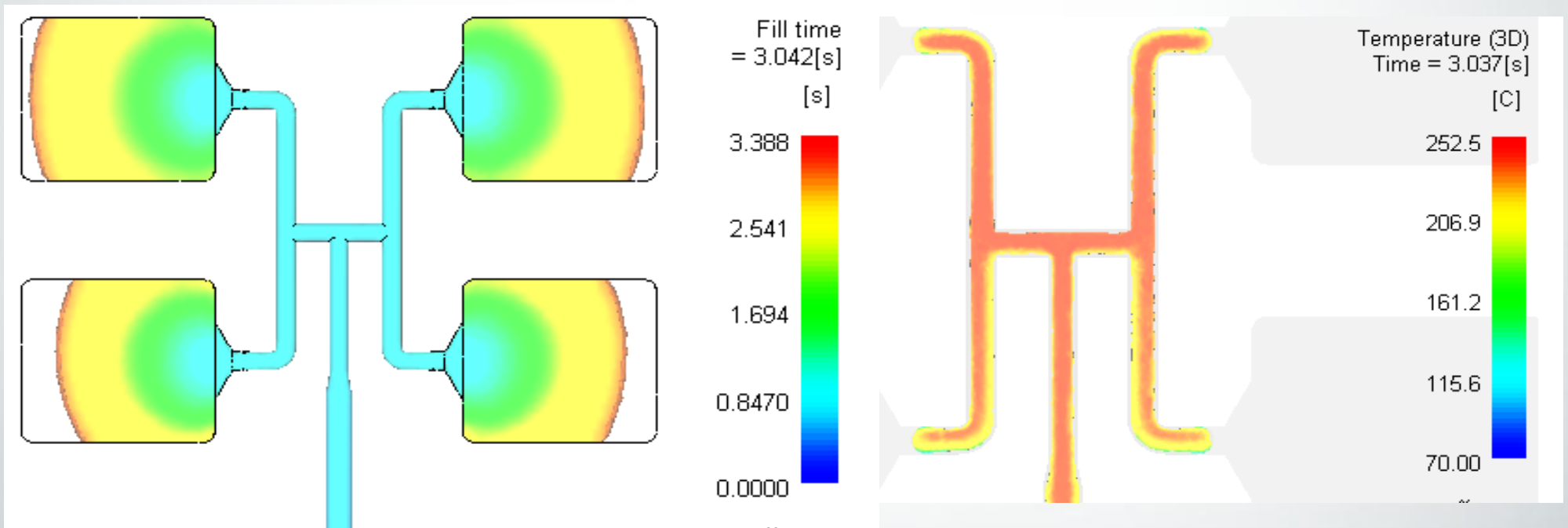
Runner imbalance: Short shot weights

- Shear imbalance depends on injection rate
- Slower injection rates results in opposite imbalance due to cooling effect



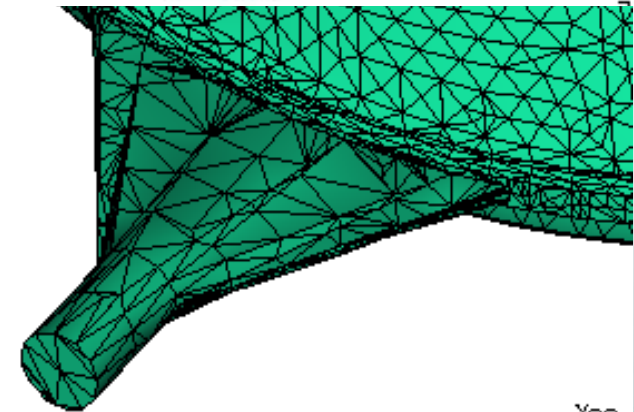
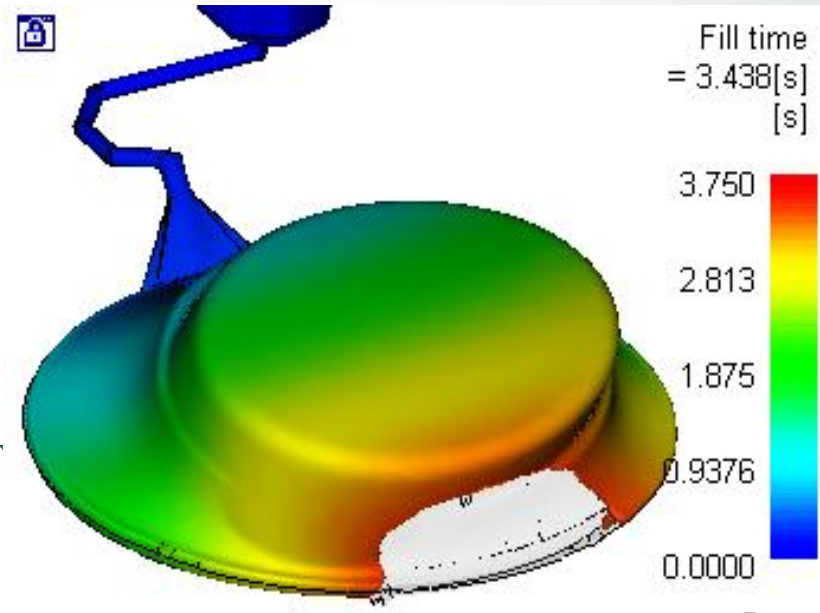
Runner imbalance: Slow injection

- Slow injection rate



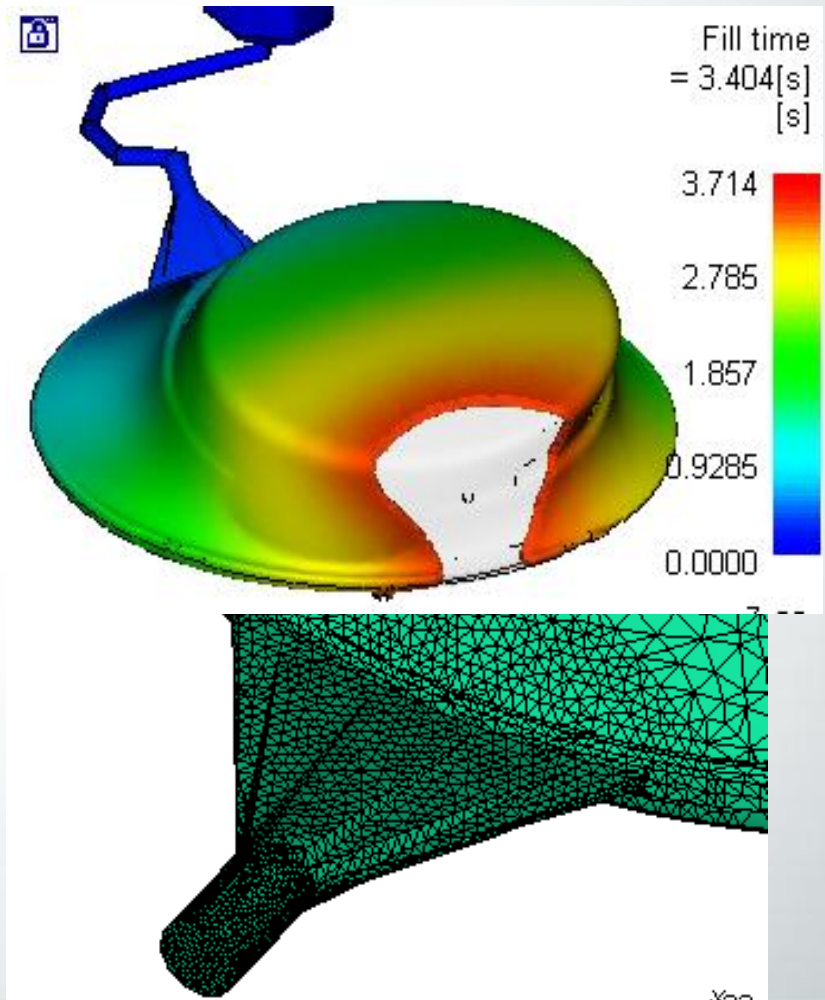
Edge flow in PC lens: Fill pattern

- Initial analysis does not agree with molding short shot



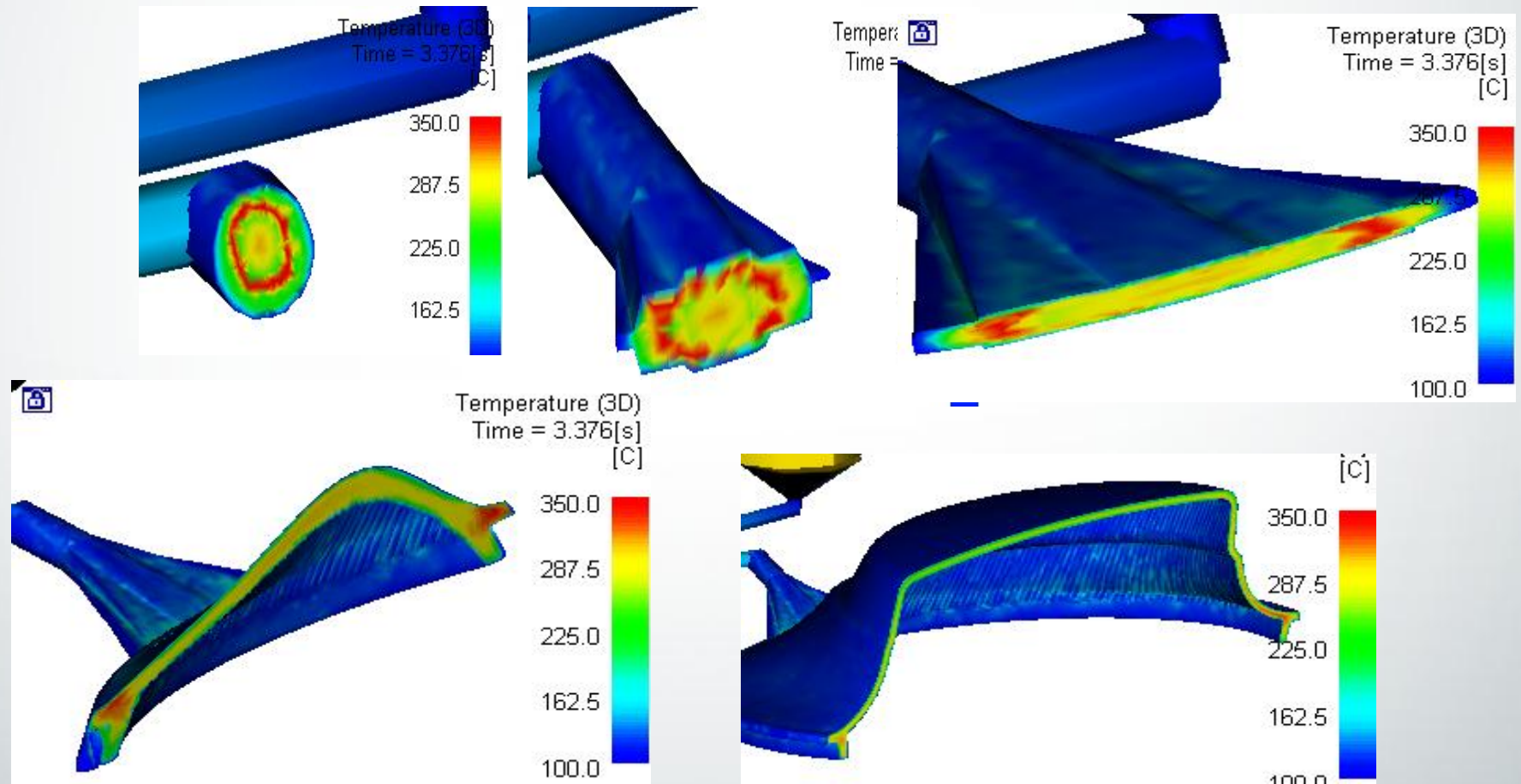
Edge flow in PC lens: Fill pattern (2)

- Refined gate at mesh gives better agreement



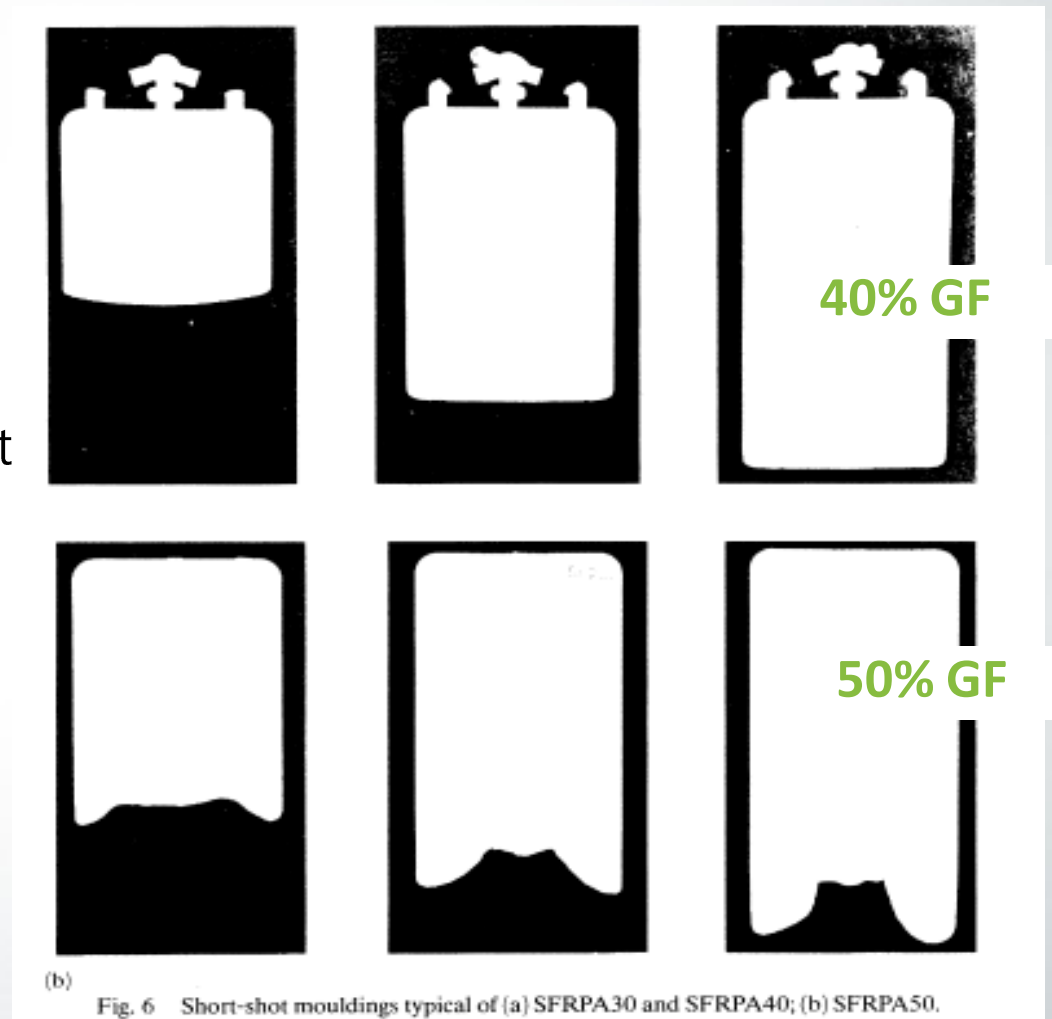
Edge flow in PC lens: Temperature slice

- Temperature distribution in the runner and gate



Ear-flow in fiber filled materials

- Akay & Barkley*
 - Increasing the fiber content caused advanced flow at the edge
 - Maranyl A690 (PA)
 - Possibly due to fiber alignment and effect on viscosity



*Plastics, Rubber and Composites Processing and Applications
Vol 20 (3), 1993. pp137-149

Content

■ Autodesk Simulation Overview

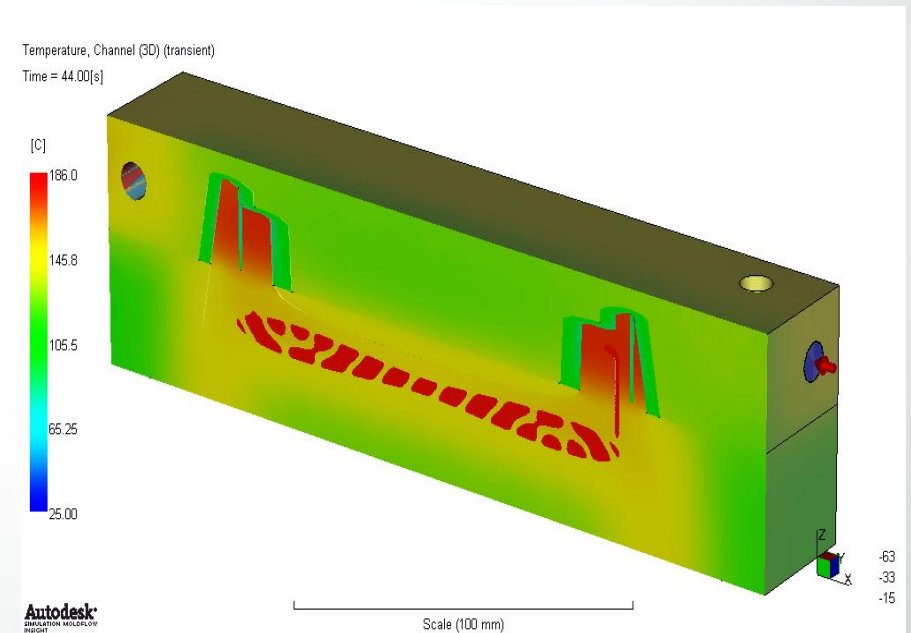
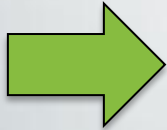
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■ Some Recent Advances

- Long Fiber Breakage
- Crystalline Morphology
- Stress Relaxation

■ Some Tough Problems

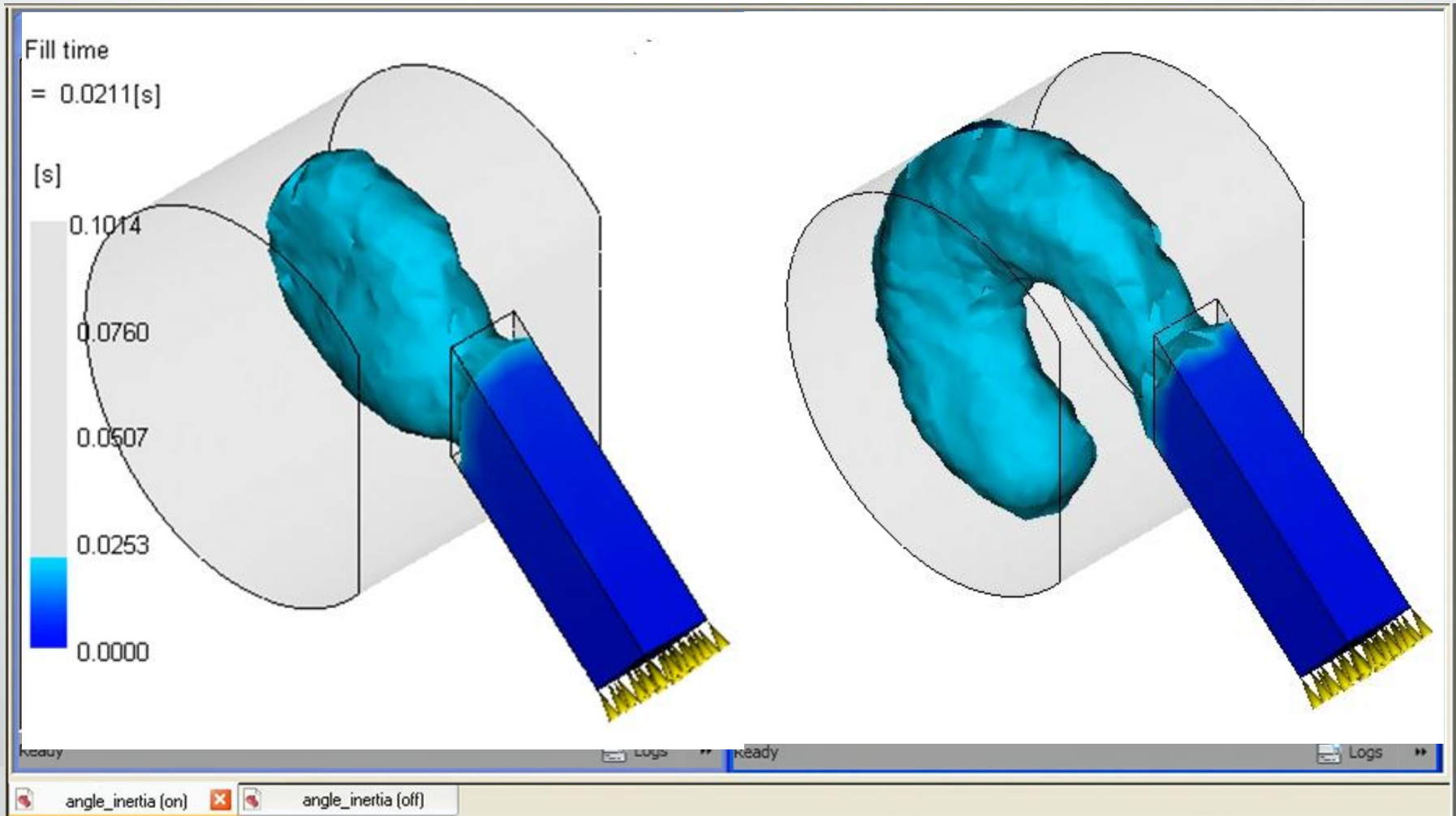
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Wall-Slip for 3D Flow

No Slip

With Slip



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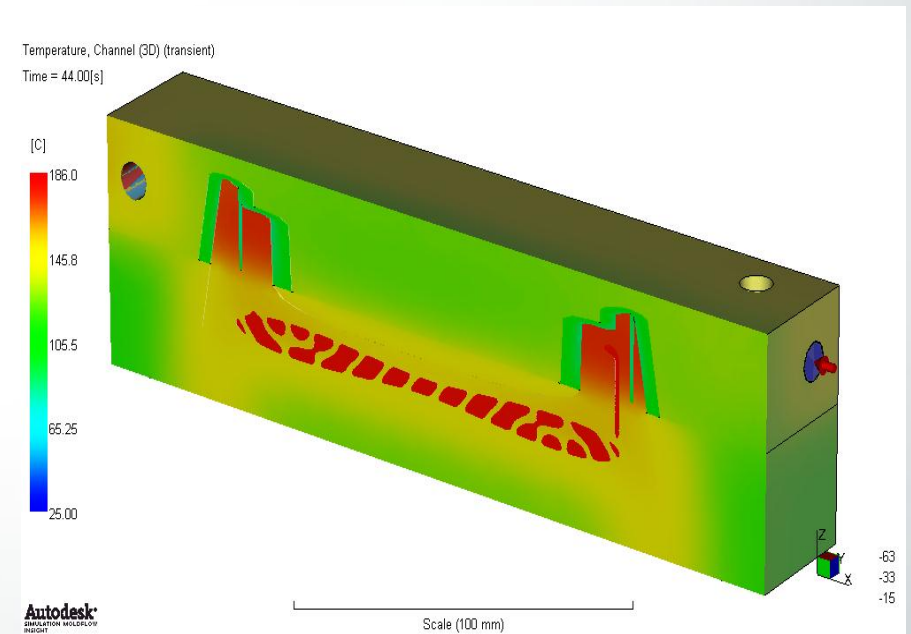
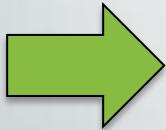
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Tiger Stripes

- Caused by a viscoelastic flow instability?

